



μFLOW CELL
Scaling Microfluidics to
Industrial Applications



VRIJE
UNIVERSITEIT
BRUSSEL

Microfluidic principles

Basic principles

Wim De Malsche

μFlow, Department of Chemical Engineering
Vrije Universiteit Brussel

Séverine Le Gac

Applied Microfluidics for BioEngineering Research (AMBER)
MESA+ Institute for Nanotechnology
MIRA Institute for Biomedical Engineering and Technical Medicine
University of Twente

Content and scope of the course

Outline

- Basics of fluid dynamics
- Existence of different types of flow regimes
 - Laminar vs. turbulent flow
 - How to predict the flow regime? $\Rightarrow$ Reynolds number (Re)
- Laminar flow: properties
- Mixing under laminar flow conditions
- Diffusion phenomena
- **Pumping in microfluidic systems**
 - Hydrodynamic pumping (pressure-driven pumping)
 - Electro-driven pumping
 - Other pumping strategies
- **Laminar flow** platforms (continuous flow)
- **Droplet** platforms (discrete/segmented flow)

Fluid dynamics - basics

- Navier Stokes equation (conservation of impulse)

$$\rho \left(\frac{\partial \vec{v}}{\partial t} + (\vec{v} \cdot \nabla) \vec{v} \right) = -\nabla \vec{p} + \mu \nabla^2 \vec{v} + \vec{F}$$

Acceleration Convective acceleration Pressure gradient Viscous forces External forces

v : flow component in x-direction
also equations for y- and z-direction

“Simplified” expression

$$\vec{0} = -\nabla \vec{p} + \mu \nabla^2 \vec{v}$$

- Steady flow, no external forces applied on the liquid
- Viscous regime

Fluid dynamics - basics

- **Conservation of mass (continuity equation, liquid)**

$$\frac{\partial \rho}{\partial t} + \operatorname{div}(\rho \mathbf{u}) = 0$$

For incompressible fluids $\partial \rho / \partial t = 0$, and the equation becomes:

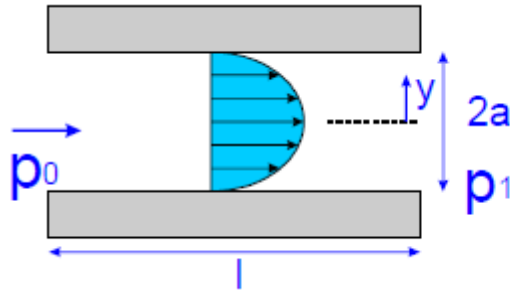
$$\operatorname{div} \mathbf{u} = 0.$$

Alternative ways to write this: $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$ and $\frac{\partial u_i}{\partial x_i} = 0$

- **Convection-diffusion equation (species in liquid)**

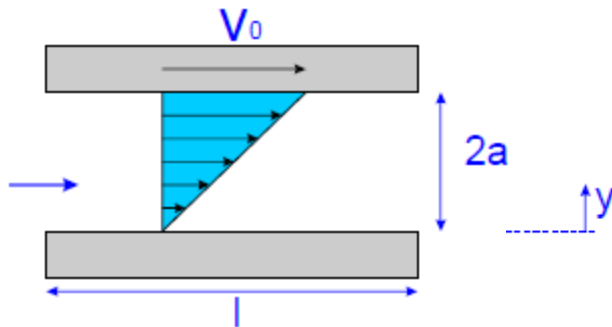
Steady state flow profiles

- Pressure-driven flow (Poiseuille flow)



$$v(y) = \frac{-1}{2\eta} (y^2 - a^2) \frac{dP}{dx}$$

- Shear-driven flow (Couette flow)



$$v(y) = \left(\frac{y + a}{2a} \right) v_0$$

Hydraulic resistance of common channel geometries

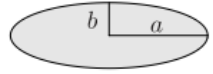
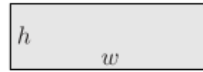
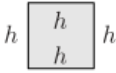
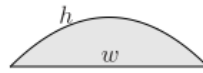
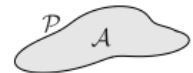
Constant $\Delta P \rightarrow$ constant flow rate Q

$$\Delta P = R_{hyd} Q$$

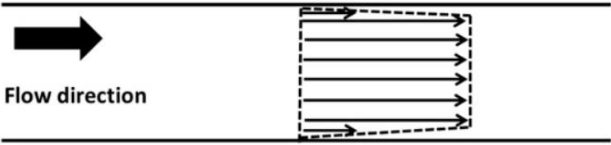
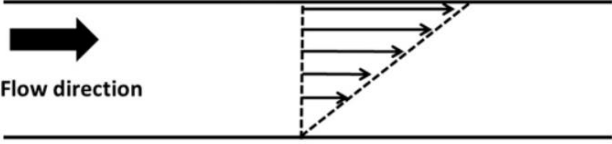
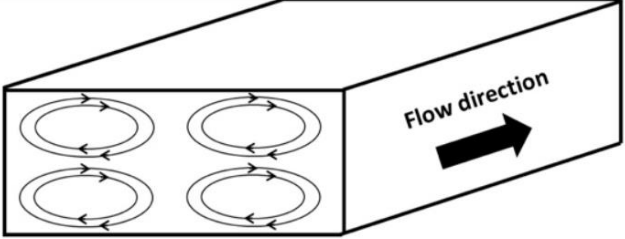
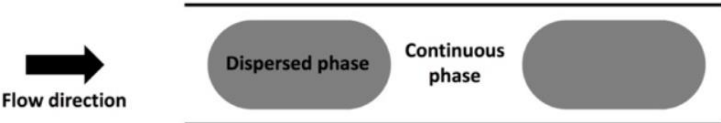
Analogy with Ohm's law:

$$\Delta V = R I$$

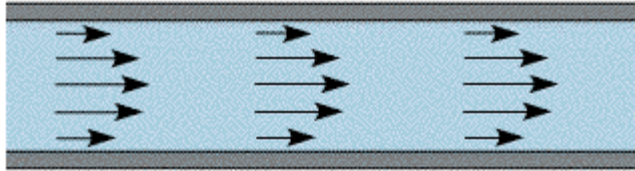
Table 4.1 A list over the hydraulic resistance for straight channels with different cross-sectional shapes. The numerical values are calculated using the following parameters: $\eta = 1 \text{ mPa s}$ (water), $L = 1 \text{ mm}$, $a = 100 \text{ }\mu\text{m}$, $b = 33 \text{ }\mu\text{m}$, $h = 100 \text{ }\mu\text{m}$, and $w = 300 \text{ }\mu\text{m}$.

shape		R_{hyd} expression	R_{hyd} [$10^{11} \frac{\text{Pa s}}{\text{m}^3}$]	reference
circle		$\frac{8}{\pi} \eta L \frac{1}{a^4}$	0.25	Eq. (3.39b)
ellipse		$\frac{4}{\pi} \eta L \frac{1 + (b/a)^2}{(b/a)^3} \frac{1}{a^4}$	3.93	Eq. (3.38)
triangle		$\frac{320}{\sqrt{3}} \eta L \frac{1}{a^4}$	18.5	Eq. (3.46)
two plates		$12 \eta L \frac{1}{h^3 w}$	0.40	Eq. (3.30)
rectangle		$\frac{12 \eta L}{1 - 0.63(h/w)} \frac{1}{h^3 w}$	0.51	Eq. (3.58)
square		$28.4 \eta L \frac{1}{h^4}$	2.84	Exercise 4.4
parabola		$\frac{105}{4} \eta L \frac{1}{h^3 w}$	0.88	Eq. (3.80)
arbitrary		$\approx 2 \eta L \frac{P^2}{A^3}$	–	Eq. (3.27a)

Overview flow profile toolbox

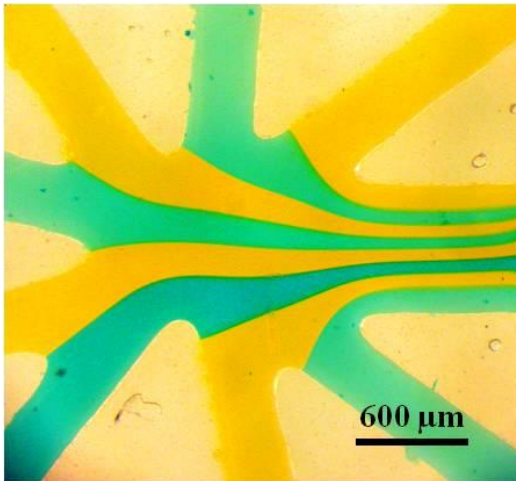
Plug flow	
Constant shear	
Linear shear	
Vortical flow	
Segmented flow	

Laminar vs. turbulent flow

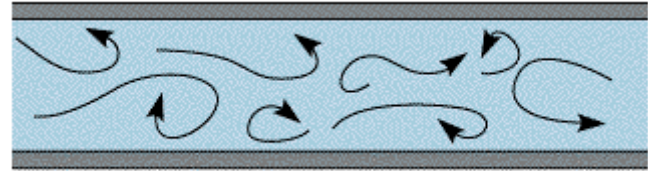


Laminar flow

Predictable, organized, deterministic

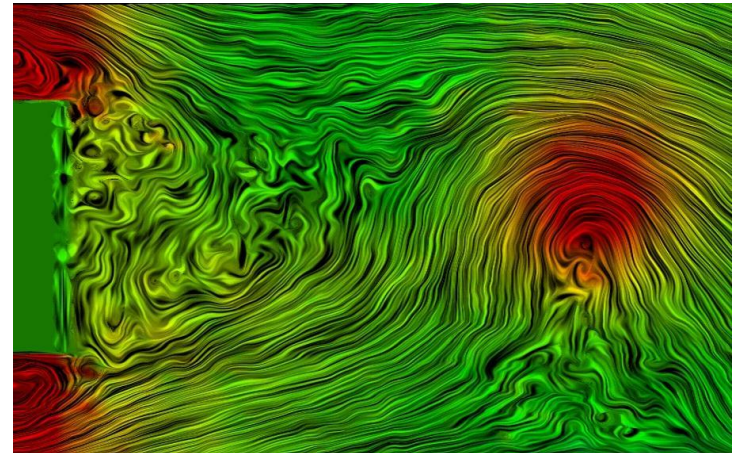


<http://alcheme.tamu.edu>



Turbulent flow

Chaotic, unpredictable, disorganized



<http://www.math.rug.nl/>

⇒ When do we have a laminar flow? When do we have a turbulent flow?

Laminar vs. turbulent flow

⇒ When do we have a laminar flow? When do we have a turbulent flow?



Laminar flow

When?

- High viscosity
- Small dimensions
- Low flow-rate/velocity



Turbulent flow

When?

- Low viscosity
- Large dimensions
- High flow-rate/velocity

Important parameters

- Viscosity of the fluid
- Dimension of the flow
- Flow velocity / flow-rate

Laminar vs. turbulent flow

Reynolds number

$$Re = \frac{\rho v l}{\mu}$$

ρ density of the fluid (kg/m³)

v average flow velocity (m/s)

l characteristic length of the flow (m)

μ viscosity of the fluid (cP or kg/m.s or Pa.s)

- Dimensionless number
- Ratio between the inertial forces and the viscous forces (bulk vs. surface)
- Measure for transition between a laminar (low Re) and a turbulent flow (high Re)

Examples

1. Microsystem

$$\rho_{\text{water}} = 1000 \text{ kg/m}^3$$

$$v = 100 \text{ } \mu\text{m/s}$$

$$l = 100 \text{ } \mu\text{m}$$

$$\mu_{\text{water}} = 1 \text{ cP} = 0.001 \text{ kg/m.s}$$

$$Re = \frac{10^3 \times 100 \times 10^{-6} \times 100 \times 10^{-6}}{0.001} = 10^{-2}$$

2. Large viscous flow

$$\rho_{\text{honey}} = 1420 \text{ kg/m}^3$$

$$v = 1 \text{ cm/s}$$

$$l = 5 \text{ cm}$$

$$\mu_{\text{honey}} = 20 \text{ kg/m.s}$$

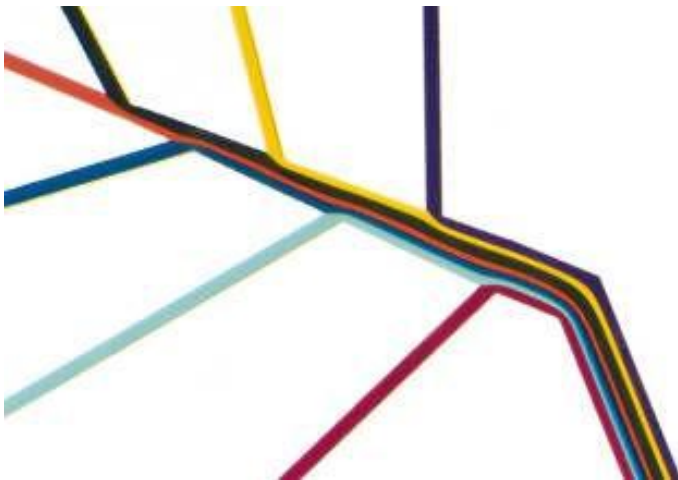
$$Re = \frac{1420 \times 10^{-2} \times 5 \times 10^{-2}}{20} = 0.035$$

Microfluidics: laminar or turbulent flow?

Microfluidics

- High surface-to-volume ratio $\Rightarrow$ surface phenomena predominant
- Small dimensions ($< 100 \mu\text{m}$)
- Low velocities ($< \text{mL/s}$)

$\Rightarrow$ **Mostly laminar flow profiles**



Kenis et al., Science 285, 83 (1999)



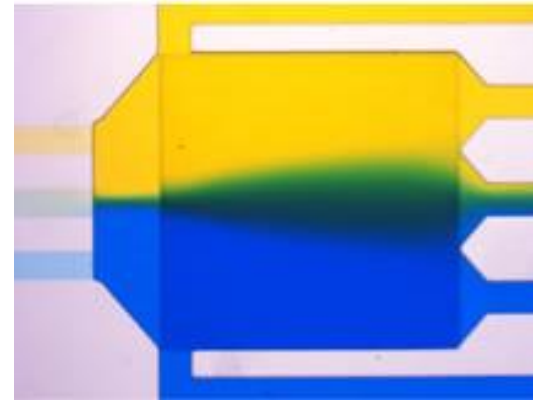
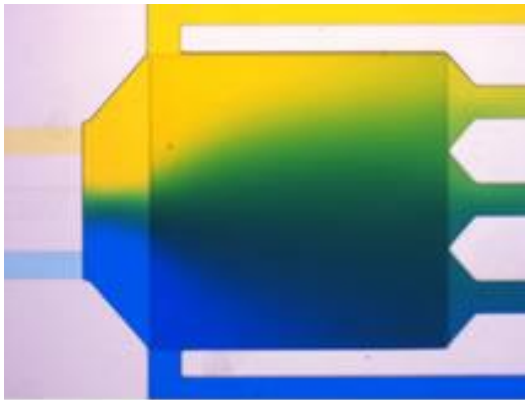
Micronics

Key-advantages

- Predictable flows, deterministic behavior
- Well-defined and controlled environment

Mixing in a laminar flow configuration?

- Mixing $\Leftrightarrow$ turbulence (active transport)
- ????? No turbulence $\Leftrightarrow$ no mixing ???



www.cellasic.com

How does mixing occur under laminar flow conditions?

$\Rightarrow$ Mixing occurs via **diffusion** of molecules between the flows (**passive transport** or “random walk”)

Diffusion

Diffusion: 1st Fick's law

$$J = -D \frac{dC}{dx}$$

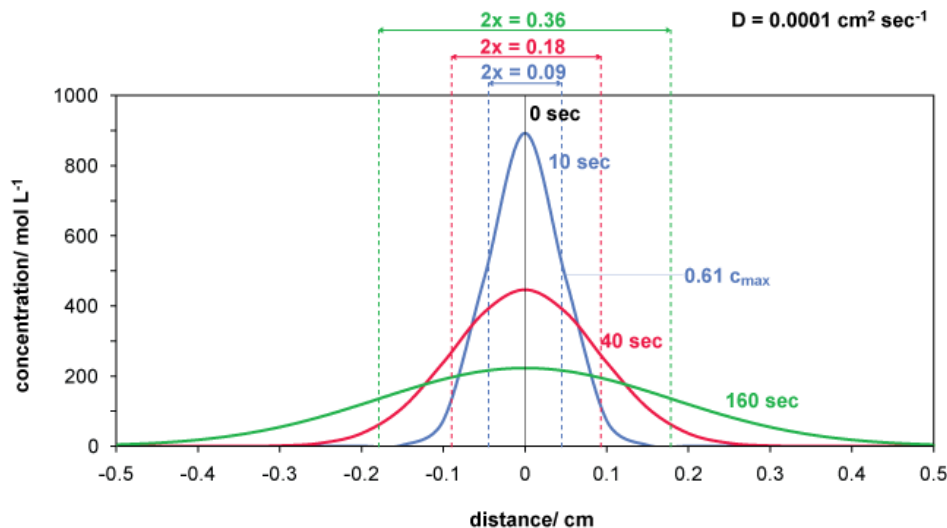
J flux of molecules (mol/m².s)

D diffusion coefficient (m²/s)

C concentration in species (mol/L or M)

⇒ The higher the concentration gradient, the more efficient the diffusive transport

Diffusion over time



Gaussian distribution

Average traveled distance

$$\bar{x} = \sqrt{2Dt}$$

Mixing by diffusion: is it efficient?

Mixing time

$$t = \frac{L^2}{2D}$$

t diffusion time (s)

L distance traveled by diffusion (m)

D diffusion coefficient (m²/s)

Examples

1. **Sugar in hot coffee** ($D \sim 8 \cdot 10^{-10}$ m²/s at 80°C; cup of ~10 cm)

$$t = \frac{(0.1)^2}{2 \times 8 \times 10^{-10}} = 6.25 \times 10^6 \text{ s} = 72 \text{ days!!!!}$$

⇒ **Better use a spoon for mixing!!!!**

2. **Small molecule in water** ($D \sim 10^{-9}$ m²/s in chemical glassware (~10 cm) and microchannel (~ 100 μm)

- $L = 10$ cm (chemical glassware) ⇒ $t = 10^7$ s!
- $L = 100$ μm (microchannel) ⇒ $t = 10$ s!

⇒ **The smaller the better!!!!**

Diffusion coefficient

Stokes-Einstein relation

$$D = \frac{k_B T}{6\pi\mu R}$$

k_B Boltzmann constant (J/K)

T temperature (K)

μ viscosity of the fluid (cP or kg/m.s)

R radius of the particle/molecule (m)

!!!!!! $\mu = f(T)$!!!!!

Examples

1. Diffusion coefficient of a virus in blood

$$k_B = 1.38 \times 10^{-23} \text{ J/K}$$

$$T = 310 \text{ K}$$

$$\mu_{\text{blood}} = 0.006 \text{ kg/m.s}$$

$$R = 50 \text{ nm}$$

$$D = \frac{1.38 \times 10^{-23} \times 310}{6\pi \times 0.006 \times 50 \times 10^{-9}} = 7.6 \times 10^{-13} \text{ m}^2/\text{s}$$

2. Diffusion coefficient of a protein in aqueous solution

$$k_B = 1.38 \times 10^{-23} \text{ J/K}$$

$$T = 298 \text{ K}$$

$$\mu_{\text{water}} = 0.001 \text{ kg/m.s}$$

$$R = 5 \text{ nm}$$

$$D = \frac{1.38 \times 10^{-23} \times 298}{6\pi \times 0.001 \times 5 \times 10^{-9}} = 4.36 \times 10^{-11} \text{ m}^2/\text{s}$$

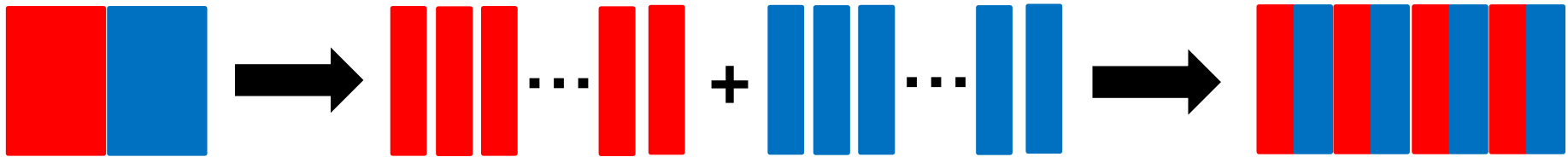
Mixing in a laminar flow configuration?



- How to improve mixing in a laminar flow configuration?

Diffusion more efficient for smaller distances

⇒ **Let's fragment the flow!**



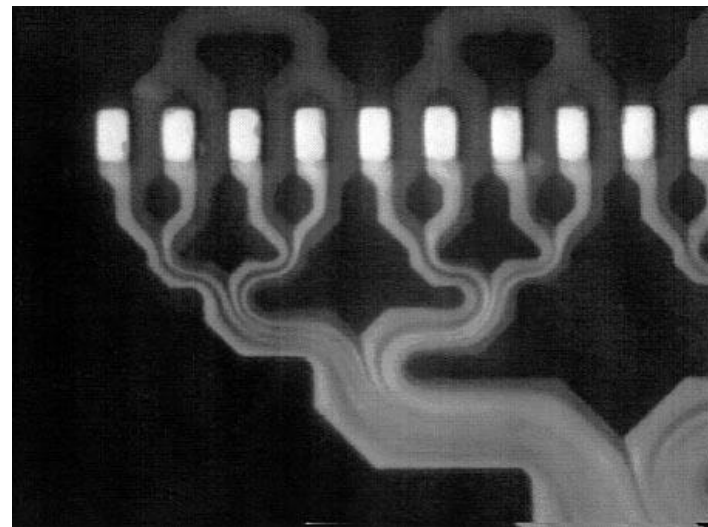
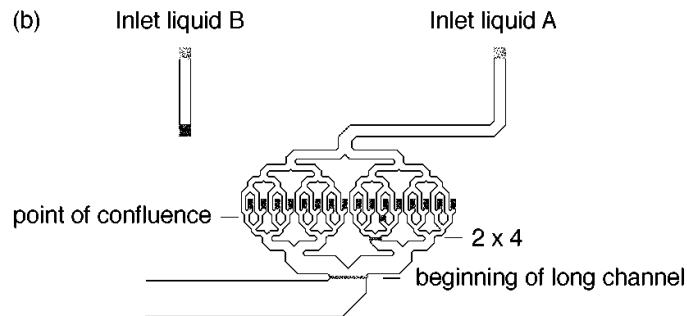
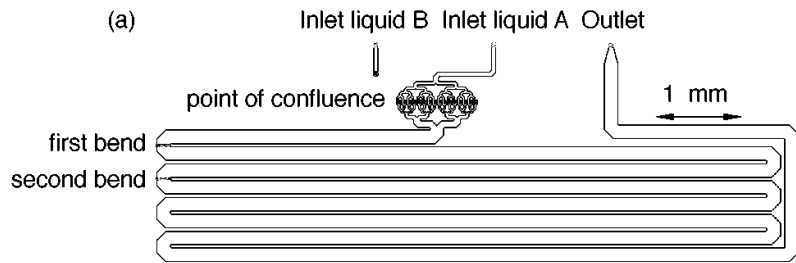
Flow divided in n sub-flows

$$L' = \frac{L}{n} \quad \longrightarrow \quad t' = \frac{L^2}{2n^2 D} \quad n = 10 \rightarrow \text{diffusion time 100 times lower!}$$

- Small molecule in water ($D \sim 10^{-9} \text{ m}^2/\text{s}$)
 - $L = 100 \text{ } \mu\text{m}$ (microchannel) $\Rightarrow t = 10 \text{ s!}$
 - If 10x fragmentations $t = 100 \text{ ms!}$

Mixing in a laminar flow configuration?

Mixing of two dyes in a fragmented flow (flow = 50 $\mu\text{L}/\text{min}$)



$t = 0$

$t = 9 \text{ ms}$

F. Bessoth et al., *Anal. Comm.* 1999, 36, 213.

Commercially available (NanoMixer, Upchurch Scientific)

Taylor-Aris dispersion



Bruus, *Theoretical microfluidics*, 2008

$$D_{ax} = D_m + \kappa \frac{v^2 d^2}{D_m}$$

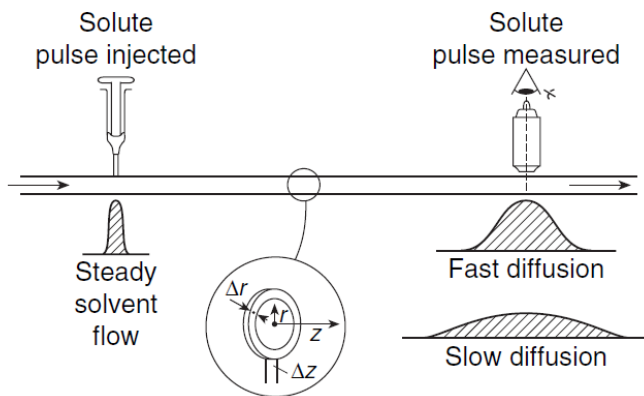
linear velocity (m/s)
channel dimension (m)

Dispersion of Soluble Matter in Solvent Flowing Slowly through a Tube

Author(s): Geoffrey Taylor

Source: *Proceedings of the Royal Society of London. Series A, Mathematical and Physical Sciences*, Vol. 219, No. 1137 (Aug. 25, 1953), pp. 186-203

Published by: Royal Society

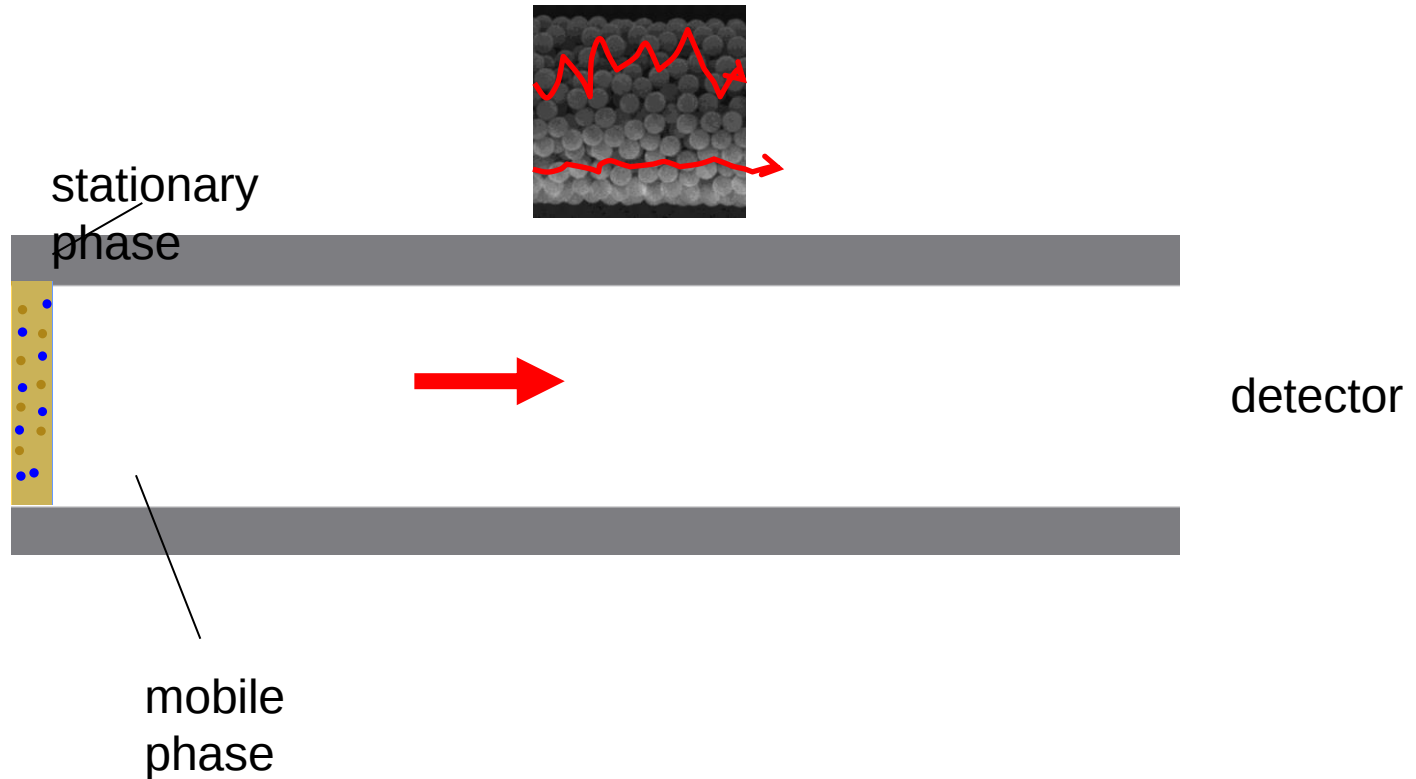


$$\kappa = \frac{1}{192} \text{ (cylinder)}$$

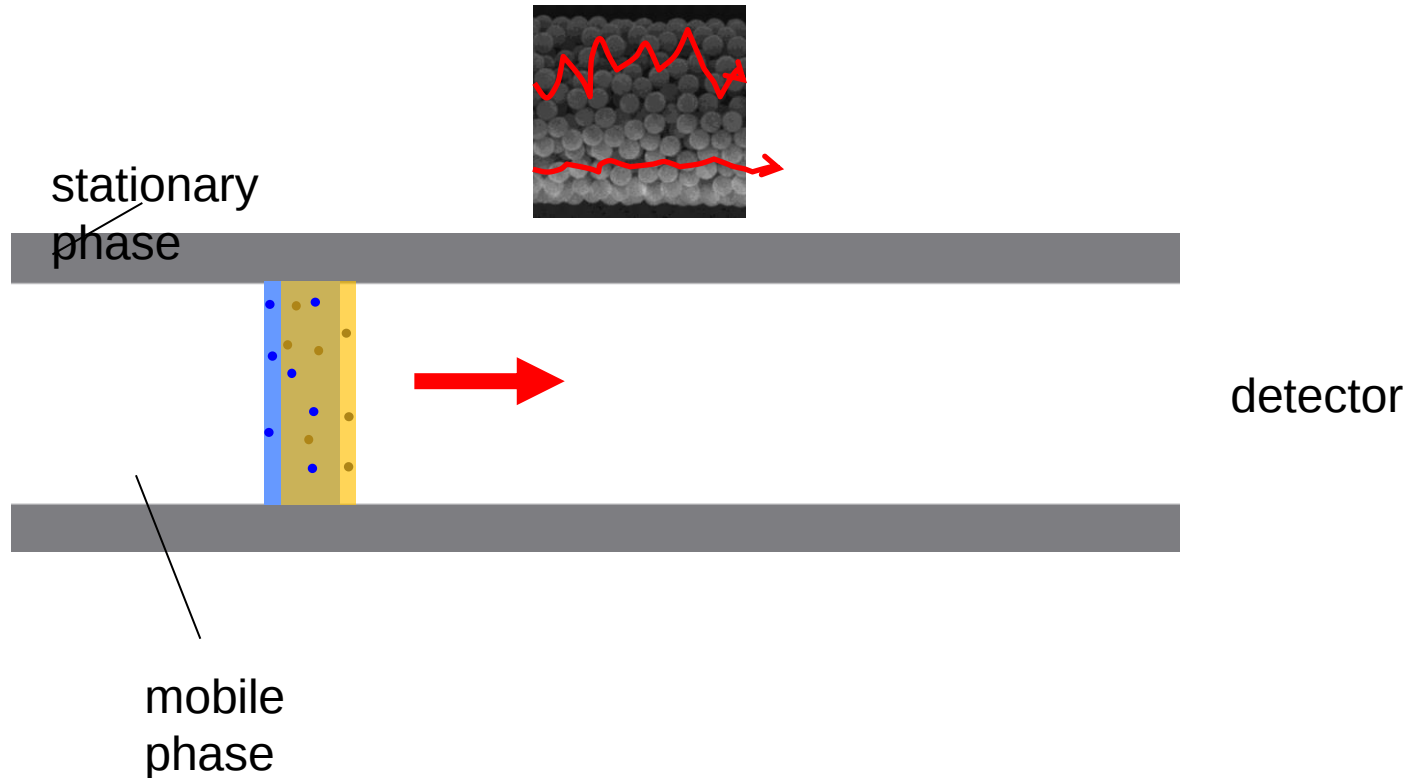
$$\kappa = \frac{1}{210} \text{ (rectangular channel)}$$

Cussler, *Diffusion*, 2009

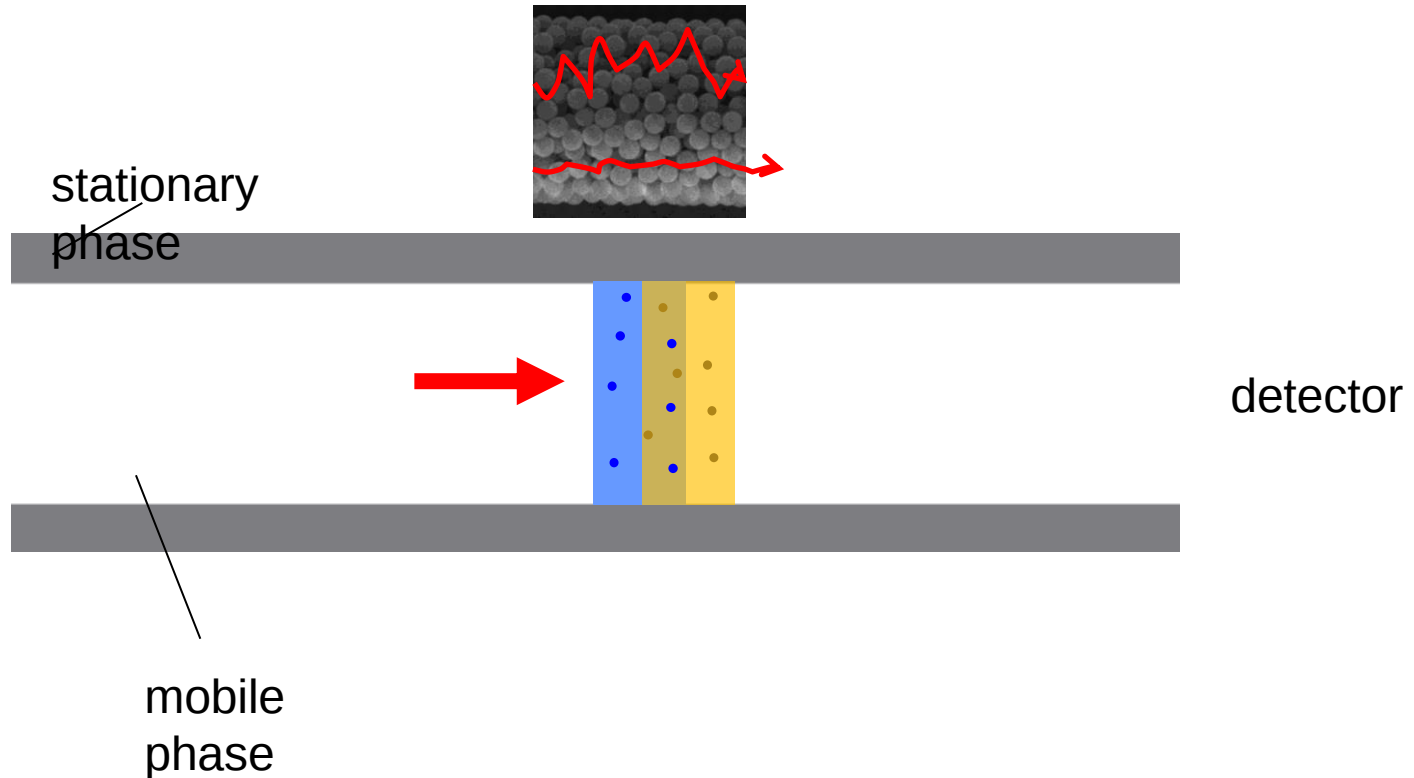
Reducing dispersion with structuring



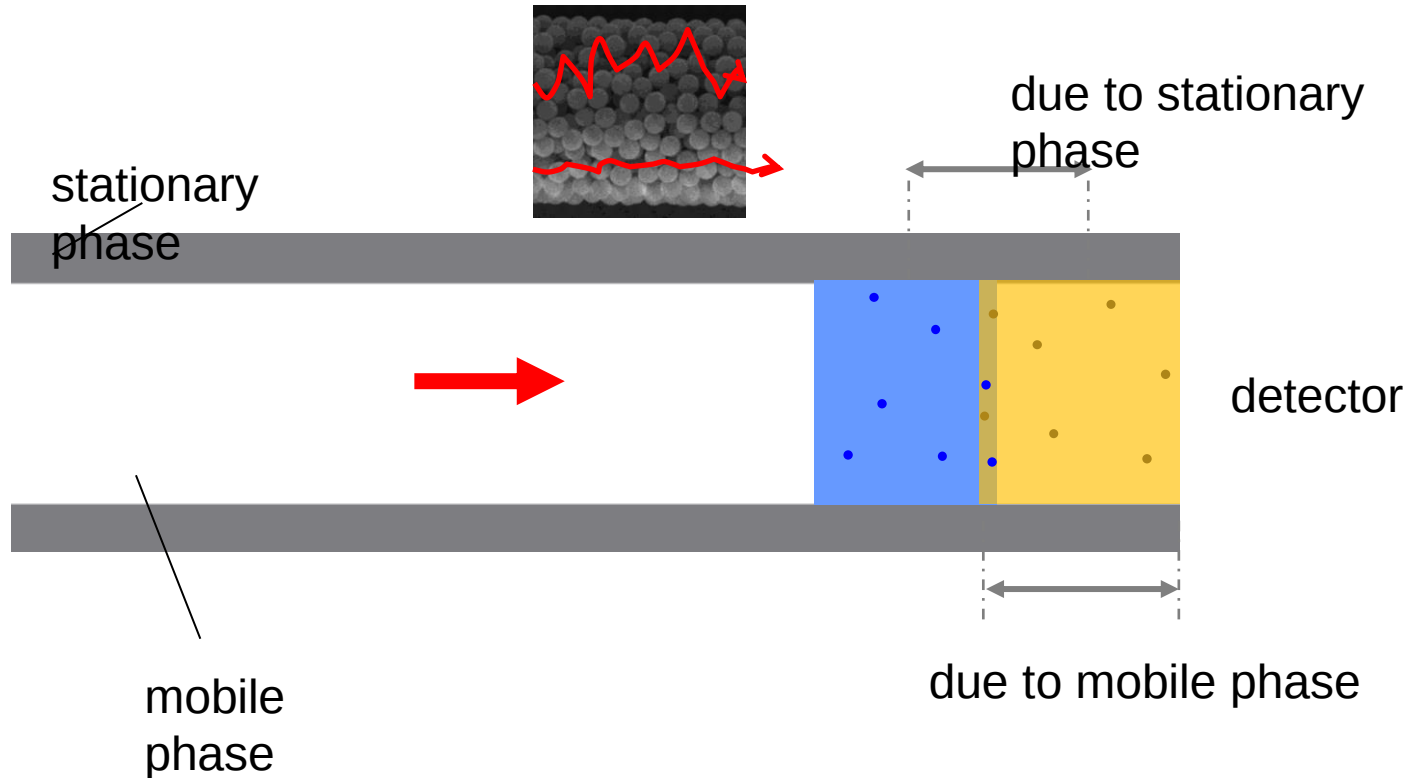
Reducing dispersion with structuring



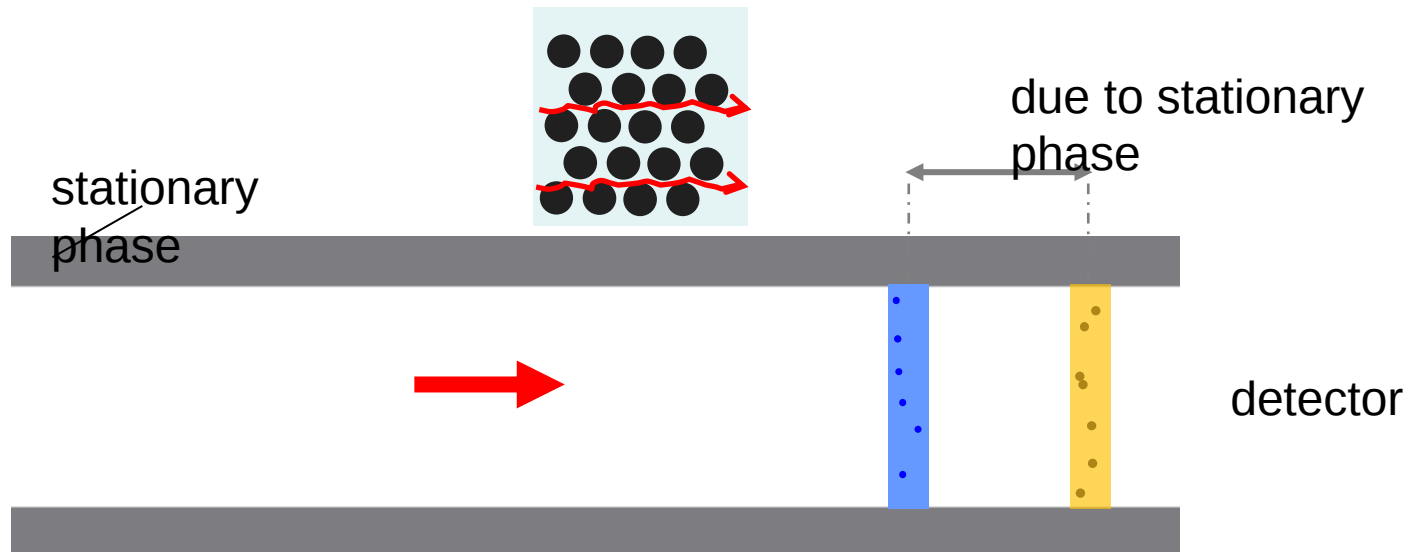
Reducing dispersion with structuring



Reducing dispersion with structuring

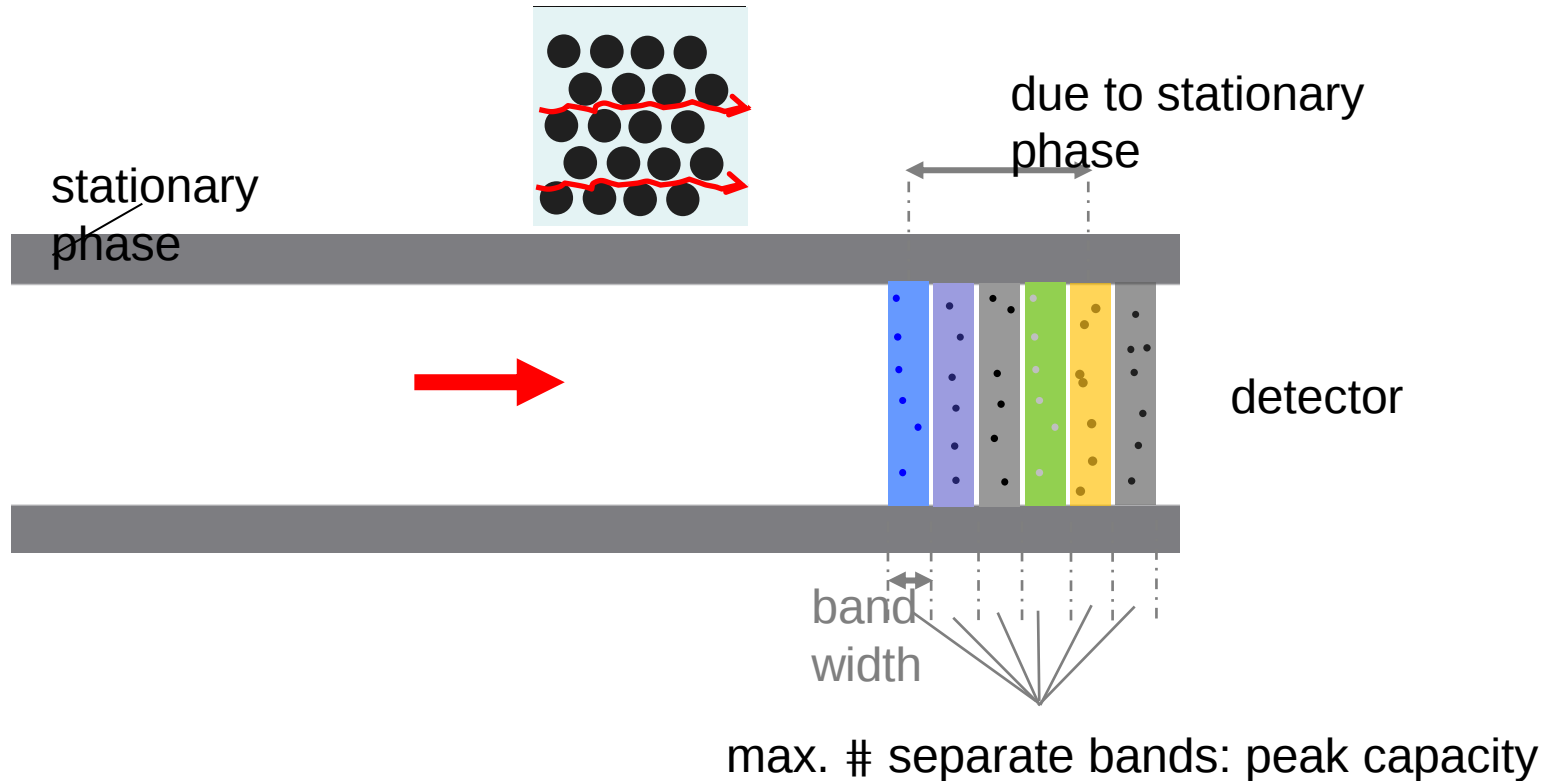


Reducing dispersion with structuring



In absence of mobile phase dispersion

Reducing dispersion with structuring

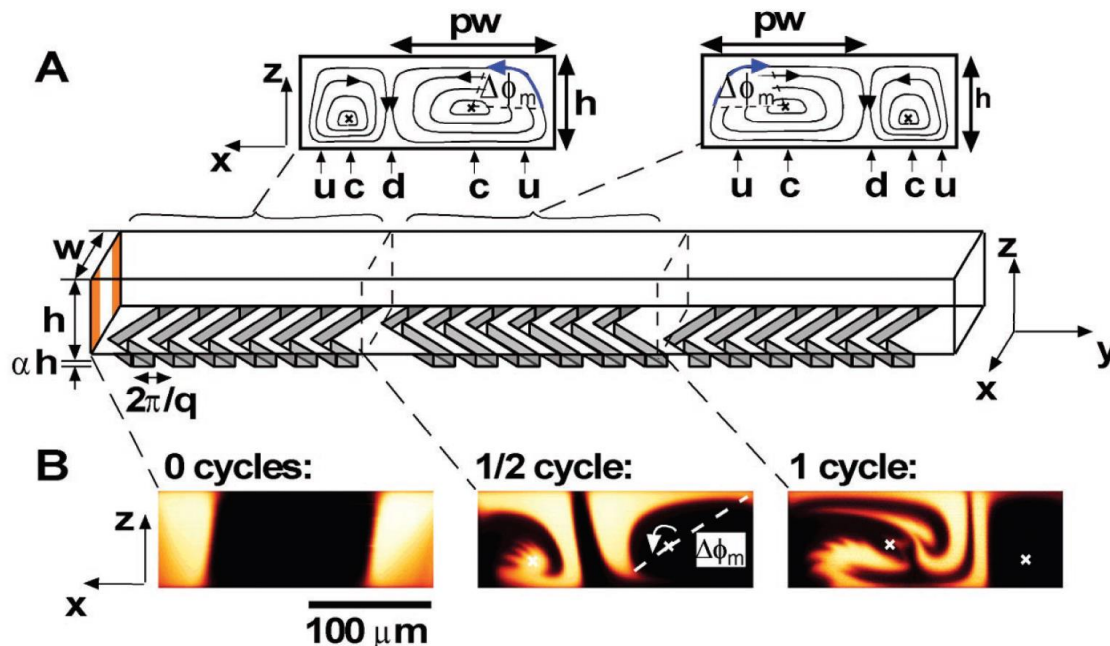


Taylor-Aris dispersion

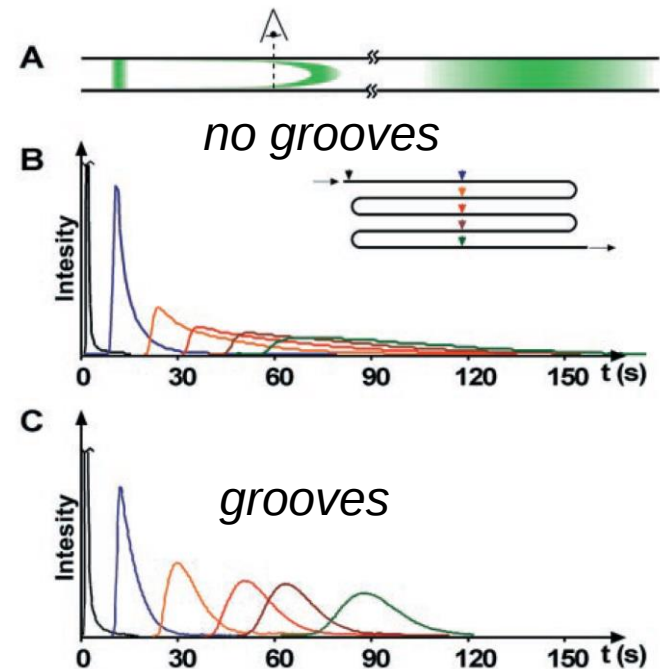
Chaotic Mixer for Microchannels

Abraham D. Stroock,^{1*} Stephan K. W. Dertinger,¹
Armand Ajdari,² Igor Mezić,³ Howard A. Stone,⁴
George M. Whitesides^{1*}

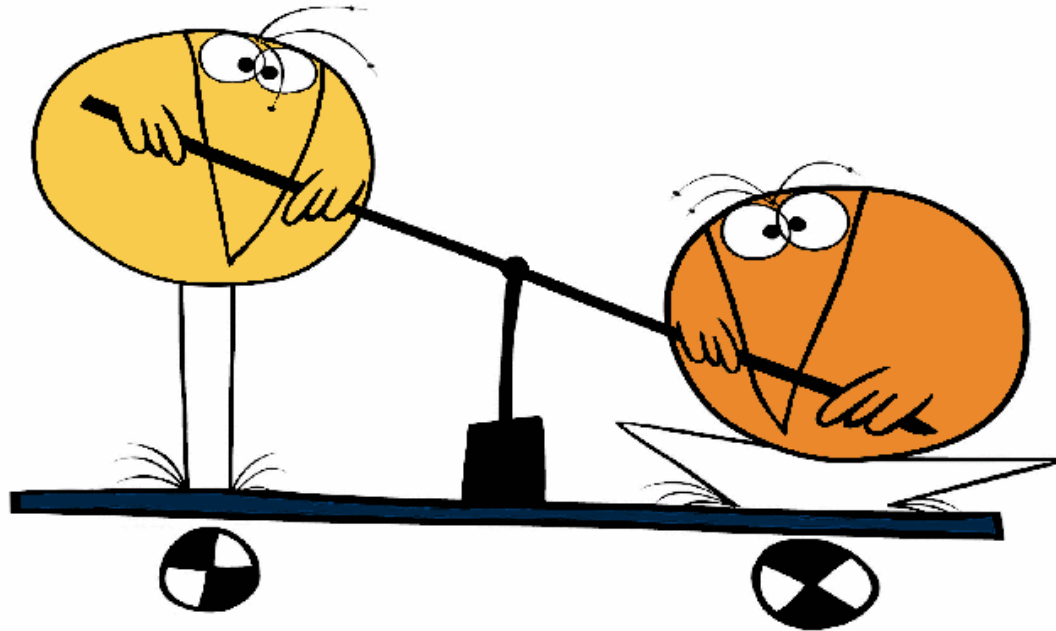
www.sciencemag.org SCIENCE VOL 295 25 JANUARY 2002



70 μm x 200 μm channel



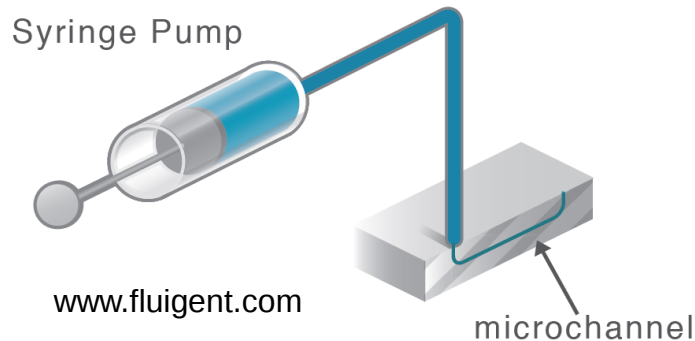
How to pump in a microfluidic device?



- How would you pump fluids in a microfluidic device?

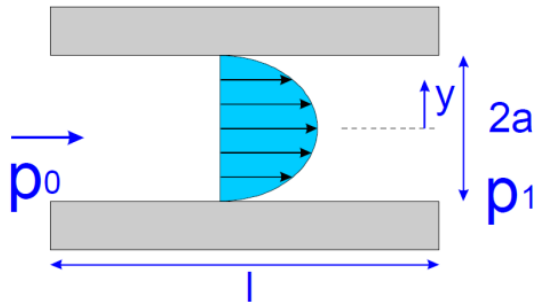
How to pump in a microfluidic device?

- **Pressure-driven flow**



- Broad range of velocities
- Suitable for any fluid

- **Parabolic flow profile**
Poiseuille flow



$$v(y) = \frac{1}{2\mu} (y^2 - a^2) \frac{dP}{dx}$$

Rect. channel ($w \gg h$): $Q = \int_0^w dy \int_0^h dz \frac{\Delta p}{2\eta L} (h - z)z = \frac{h^3 w}{12\eta L} \Delta p.$

- **Flow resistance**
Hagen-Poiseuille equation

$$R_{flow} = \frac{\Delta P}{Q} = \frac{8\mu L}{\pi r^4}$$

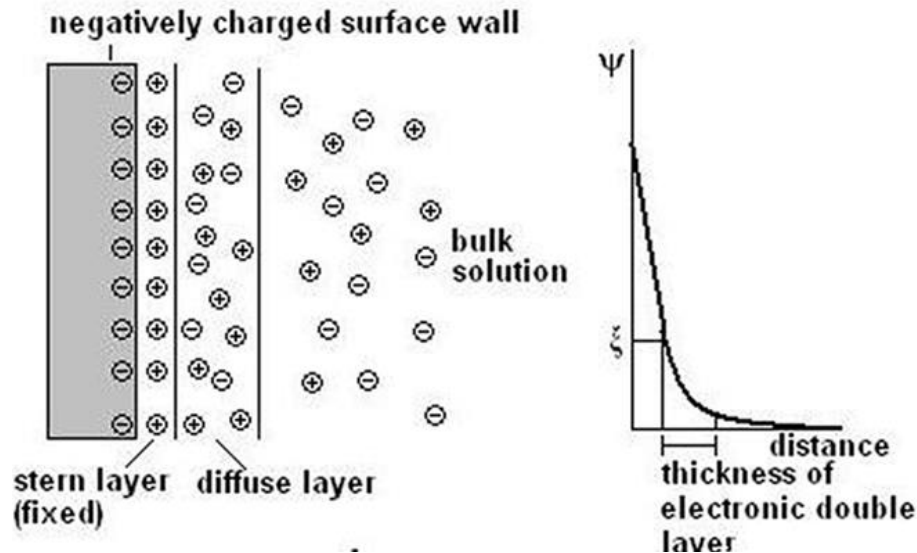
ΔP pressure drop
 Q volumetric flowrate
 μ viscosity of the fluid
 L length of the channel
 r radius of the channel

- **Parabolic flow profile:** molecular dispersion
- The smaller the channel, the higher the resistance, the higher the risk for leakages!!

How to pump in a microfluidic device?

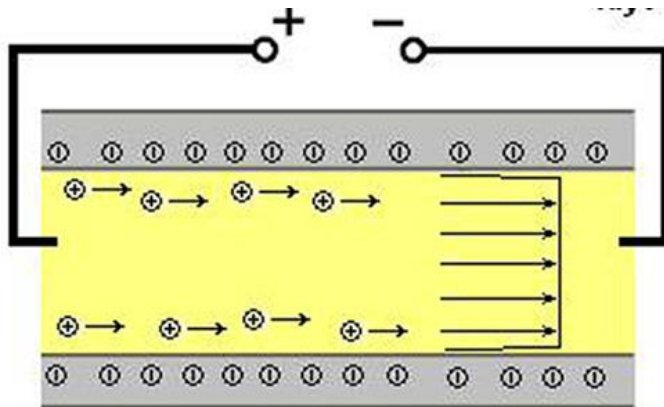
- **Electro-driven flow** (or electro-osmotic pumping)

Pumping based on surface effects only for **charged liquids**



- Capillary walls: charged (negatively)
 - ⇒ Accumulation of counter-ions at the surface
 - ⇒ Stern layer: counter-ions
 - ⇒ Diffuse layer: ions of both charges

- Application of an electric field
 - ⇒ Migration of cations towards the cathode
 - ⇒ Creation of a bulk flow towards the cathode
 - ⇒ **Electro-osmotic flow**



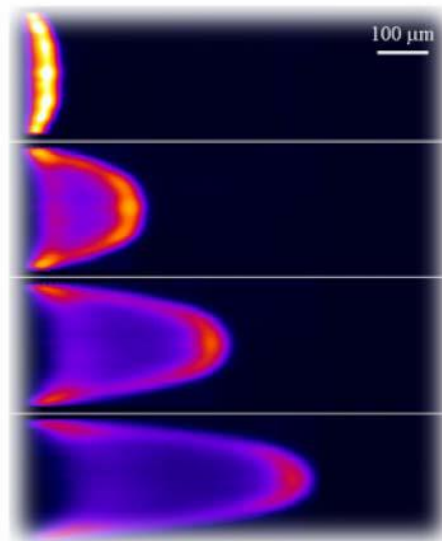
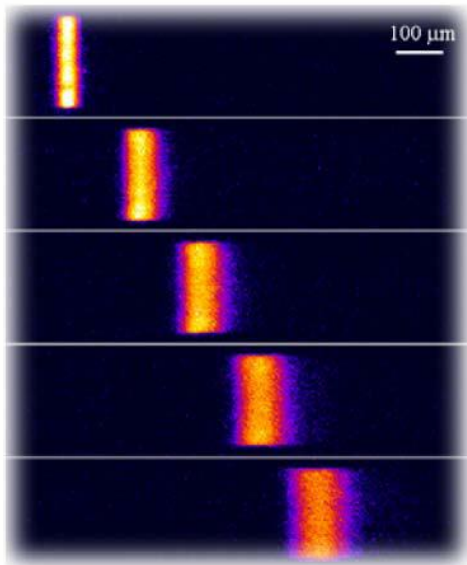
- EOF velocity: $v_{EOF} = \mu_{EOF} E$

With $\mu_{EOF} = \frac{\epsilon \xi}{\mu}$, EOF mobility; E electric field;
 ϵ dielectric constant; ξ zeta potential; μ viscosity of the fluid

How to pump in a microfluidic device?

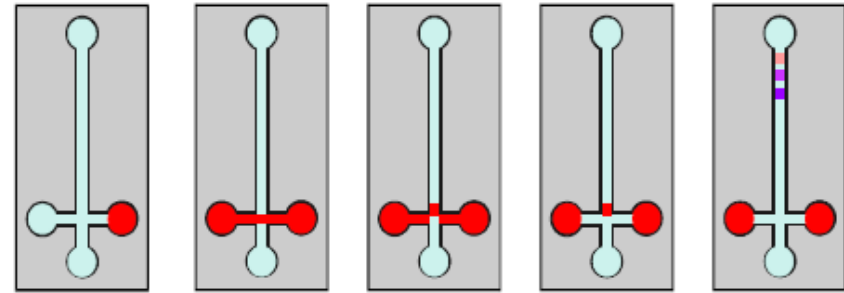
Electro-driven pumping or **EOF-pumping** (electro-osmotic flow)

- flat flow profile: plug-flow



Electro- vs. pressure-driven flow profile

liquid control $\Leftrightarrow$ switching voltages



CE-based separation in a microchip
1-2. Sample introduction;
3-4. Sample injection;
5. Sample separation

$\Rightarrow$ **Simple integration in microfluidics**

CE = capillary electrophoresis

EOF: double layer overlap

For small channels:

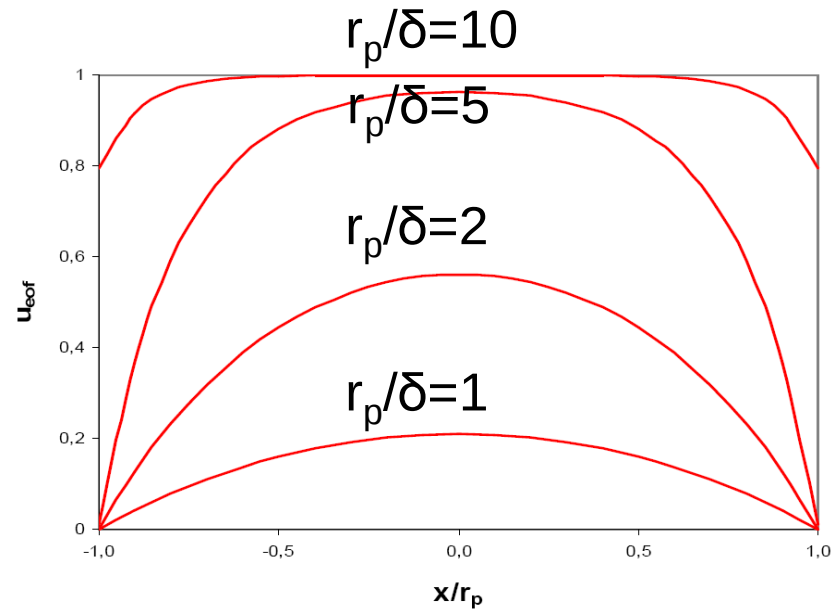
- Parabolic-like flow profile
- Significant reduction of achievable flow velocity in sub-micron channels

$$u_{\text{eof}} = \frac{\varepsilon_0 \varepsilon_e \zeta E}{\eta} \left[1 - \frac{2I_1(r_p/\delta)}{(r_p/\delta)I_0(r_p/\delta)} \right]$$

$$\delta = \sqrt{\frac{\varepsilon_0 \varepsilon_e kT}{2N_a e_0^2 C_s}}$$

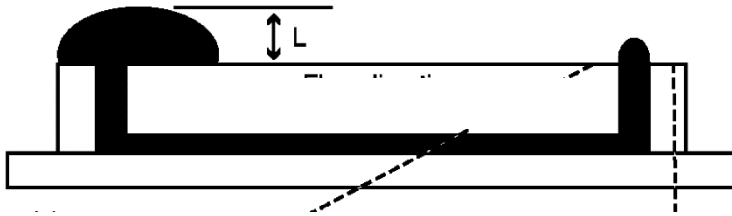
k: Boltzmann constant
 N_a : Avogadro's number
 T: temperature,
 C_s the ionic strength,
 r_p the radius of the channel
 e_0 the elementary charge unit.

C_s : the ionic strength,
 r_p : the radius of the channel
 e_0 : the elementary charge unit
 δ : double layer thickness



How to pump in a microfluidic device?

- **Passive pumping:** creation of a flow using surface tension



Interfacial pressure in droplets

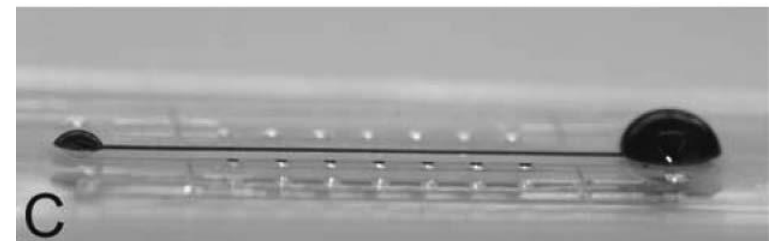
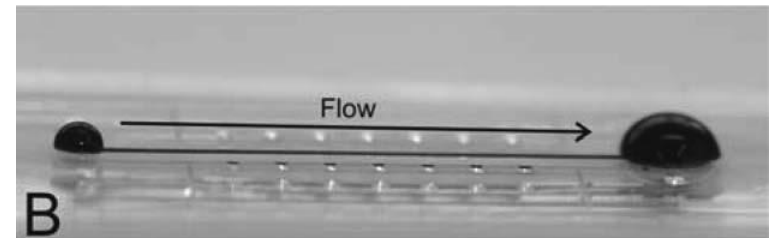
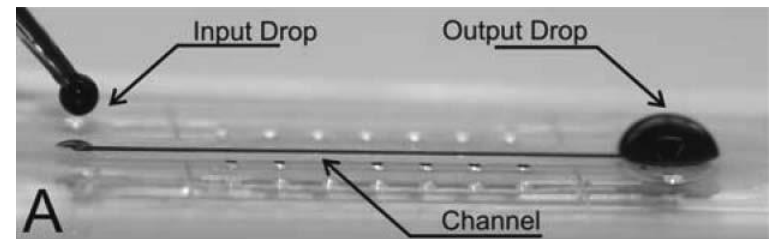
$$\Delta P = \frac{2\gamma}{R}$$

γ interfacial tension (N/m)

R radius of the droplet (m)

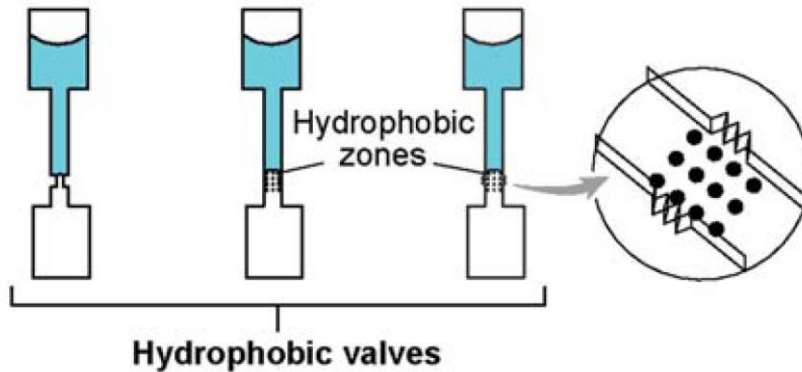
⇒ **The smaller the droplet,
the higher pressure**

- In which direction does the flow go?



How to pump in a microfluidic device?

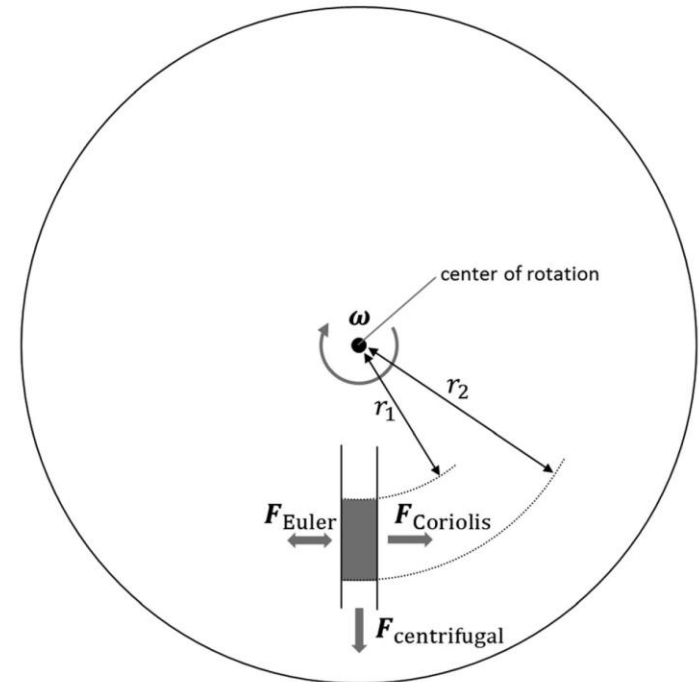
- Centrifugal pumping



Valve creation

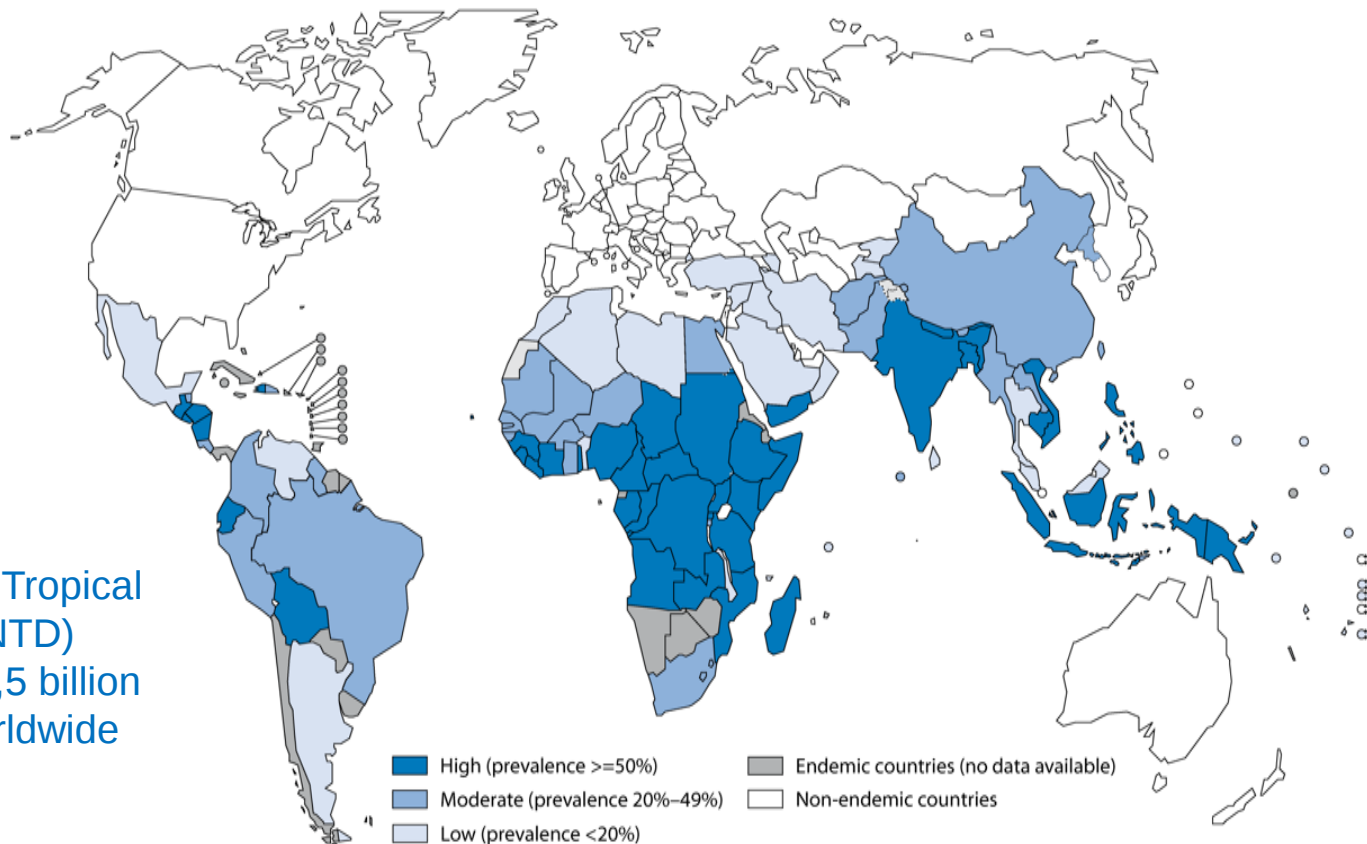
hydrophobic treatment of the surface

- Lower spinning speed: no flow
- Higher spinning speed: flow

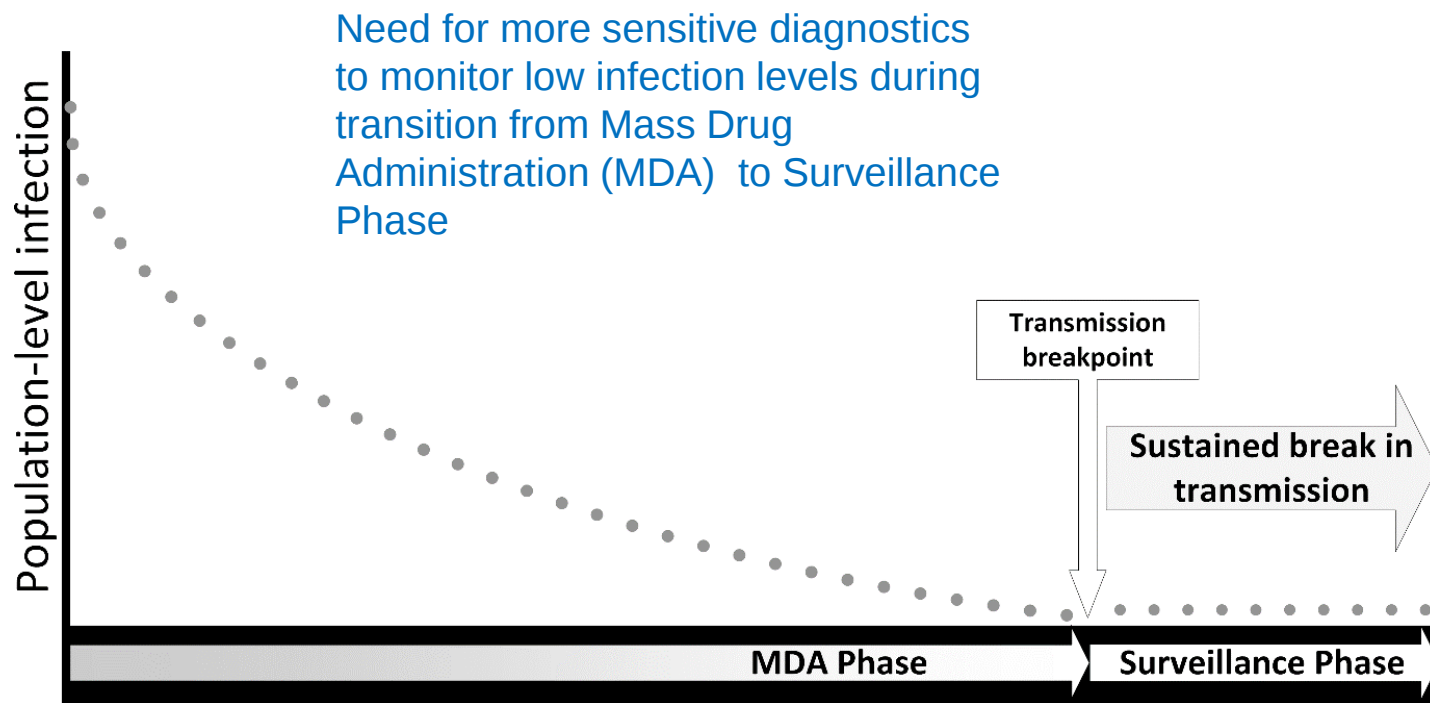


Soil Transmitted Helminth (STH) infections

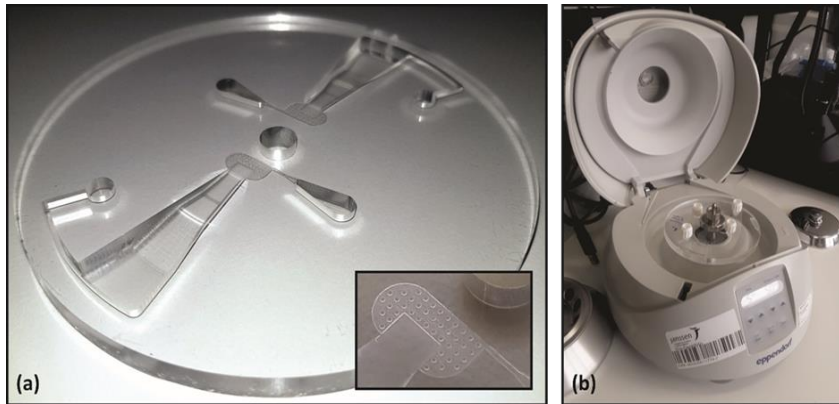
Neglected Tropical Disease (NTD)
affecting 1,5 billion
people worldwide



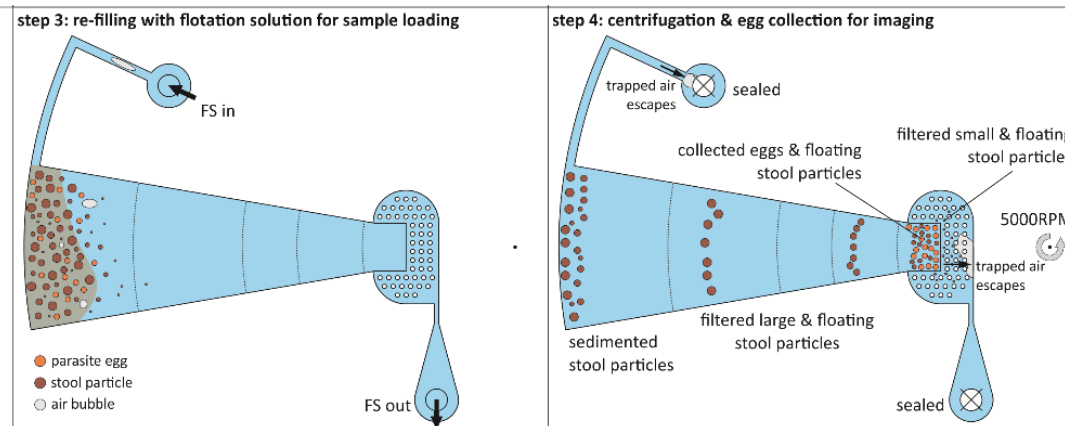
Control of STH infections



Single Image Parasite Quantification (SIMPAQ)

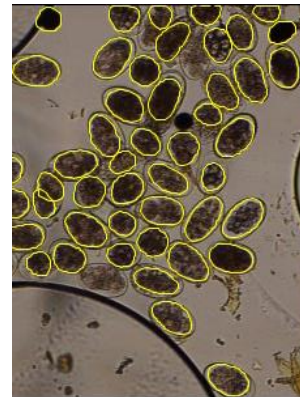
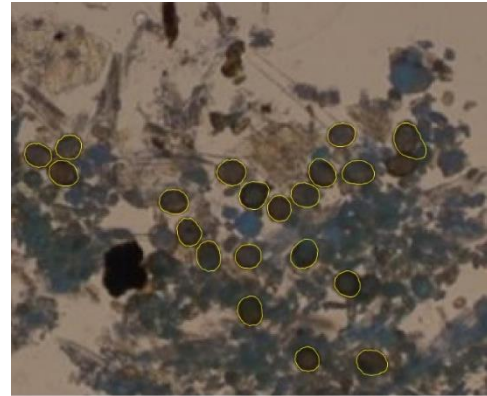


Lab-on-a-disc device using centrifugal forces to drive parasite eggs in flotation solution of stool to Field of View (FOV)



Sukas, S., Van Dorst, B., Kryj, A., Lagatie, O., De Malsche, W., Stuyver, L.J. (2019) Development of a Lab-on-a-Disk Platform with Digital Imaging for Identification and Counting of Parasite Eggs in Human and Animal Stool. *Micromachines*, 10, 852.,

Single Image Parasite Quantification (SIMPAQ)



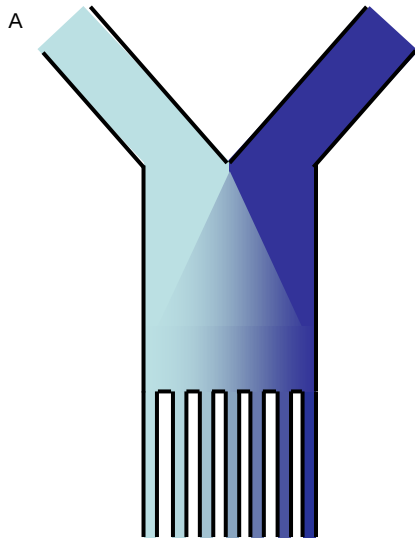
Test result captured in one picture for visual and/or automated analysis

Laminar flow platforms

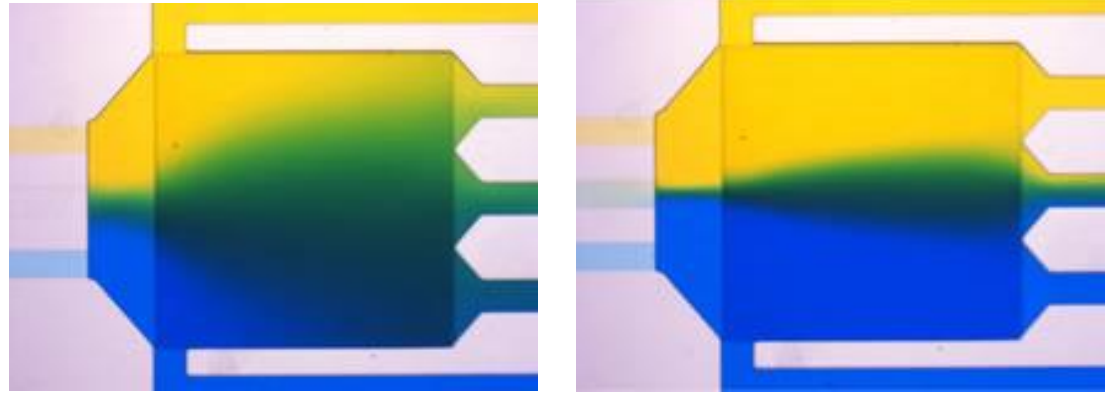


- Continuous flow microfluidic platforms
- Well-defined, deterministic flow
- Highly predictable and controlled flow
- Poor mixing efficiency
- Molecular transport solely based on diffusion

Laminar flow platforms – gradient generation



Courtesy Dr. van Uitert



www.cellasic.com

Applications

- **Cell biology:** Cells are not only responsive to the presence of certain substances but also to gradients thereof (chemotaxis).
- **Drug screening assays:** The effect of drugs is concentration-dependent and the effect of a drug must be studied for a range of concentrations.

Laminar flow platforms

- H-filter (sample purification)

- What happens if my sample input contains both large and small molecules?

Small molecules; $D = 10^{-9} \text{ m}^2/\text{s}$

$t = 1 \text{ s} \Rightarrow d_{\text{diff}} = 45 \text{ } \mu\text{m}$

$2 \text{ s} \Rightarrow 63 \text{ } \mu\text{m}$

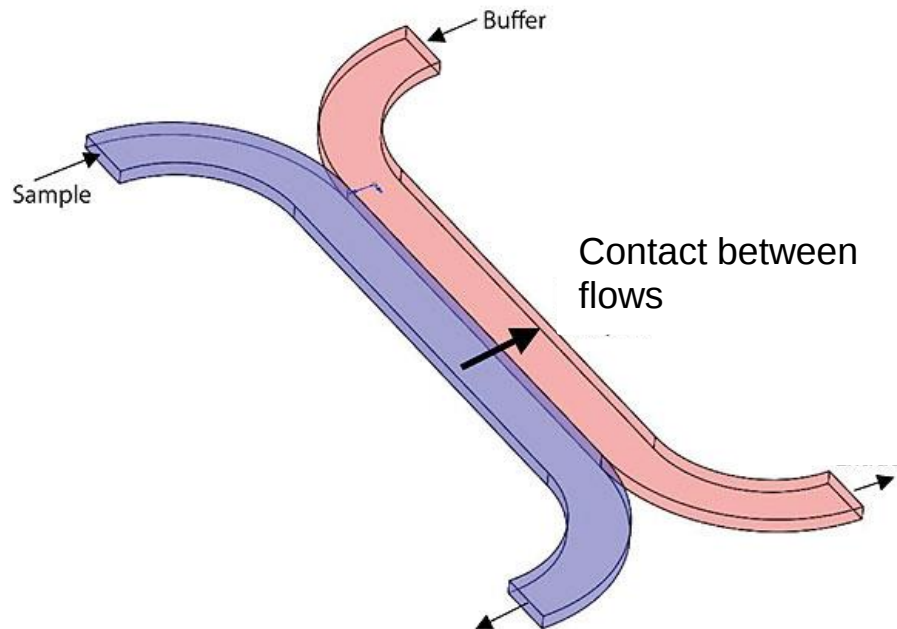
$5 \text{ s} \Rightarrow 100 \text{ } \mu\text{m}$

Large molecules (proteins); $D = 10^{-11} \text{ m}^2/\text{s}$

$t = 1 \text{ s} \Rightarrow d_{\text{diff}} = 4.5 \text{ } \mu\text{m}$

$2 \text{ s} \Rightarrow 6.3 \text{ } \mu\text{m}$

$5 \text{ s} \Rightarrow 10.0 \text{ } \mu\text{m}$

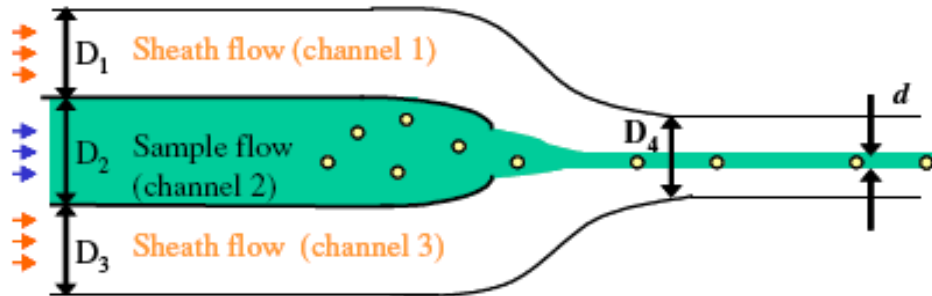


$\Rightarrow$ Removal of small particles and concentration of large particles

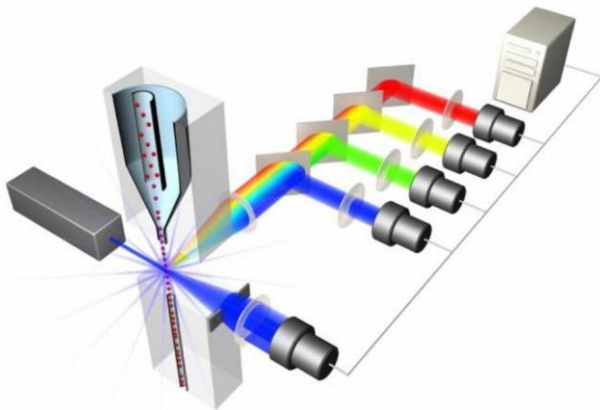
Laminar flow platforms

- Flow focusing – gel polymerisation

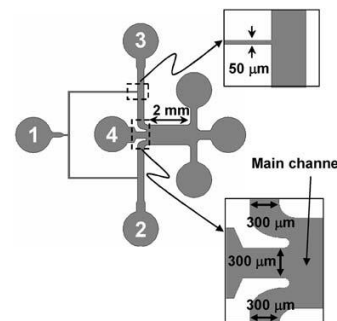
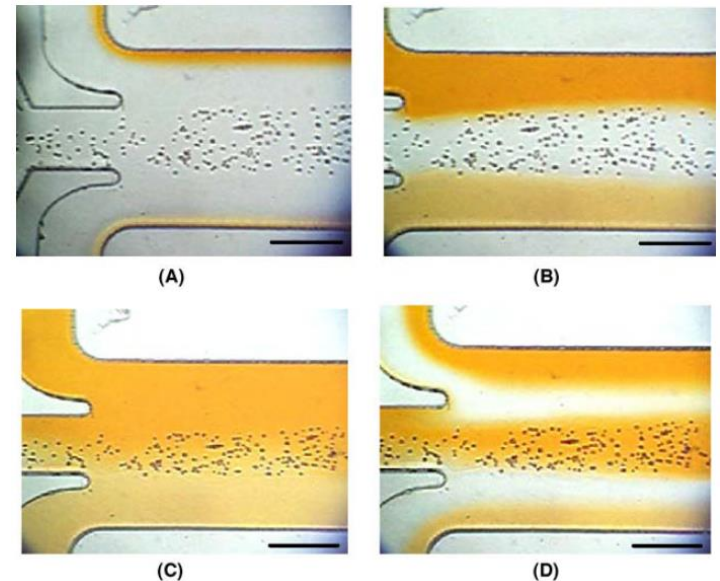
1. Hydrodynamic focusing



- Essential for cell analysis using flow cytometry
- 1 cell at a time in the flow
- Cell detection and analysis with a laser



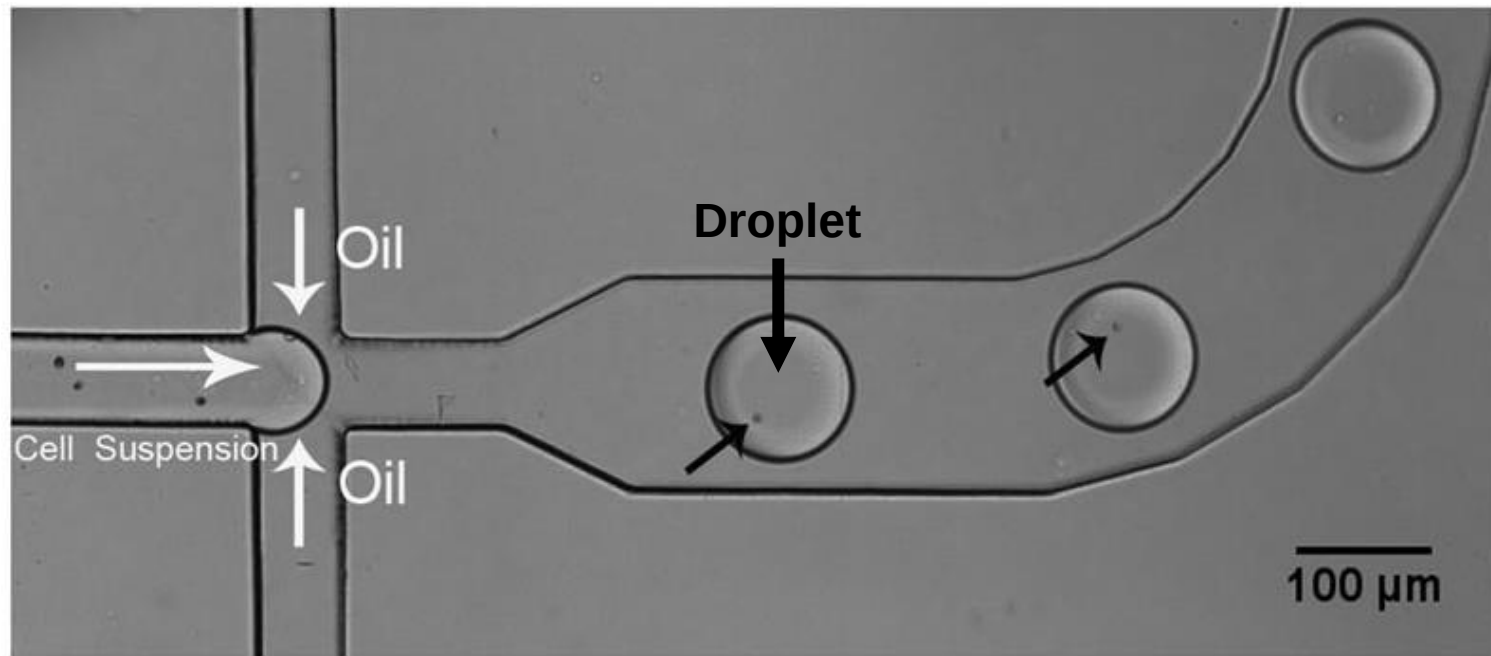
2. Gel polymerisation in a channel



In situ polymerisation of a hydrogel for cell culture in a microdevice

Droplet microfluidics

Principle: Creation of aqueous droplets (fL-nL) in a continuous oil phase (or vice/versa*)



Motivations:

- **Material sciences:** creation of a well defined emulsion $\Rightarrow$ particle synthesis with a narrow size distribution
- **Chemical & life sciences:** creation of smaller microreactors; higher reaction confinement; eventually single molecule reaction

Droplet microfluidic: generation

Capillary number

$$Ca = \frac{\mu v}{\gamma}$$

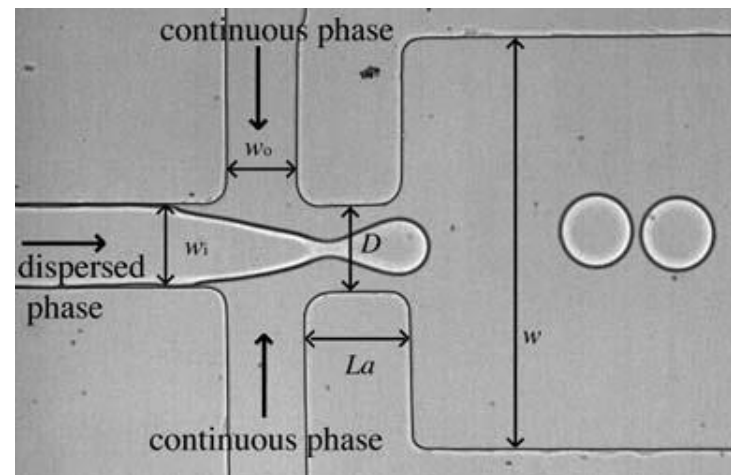
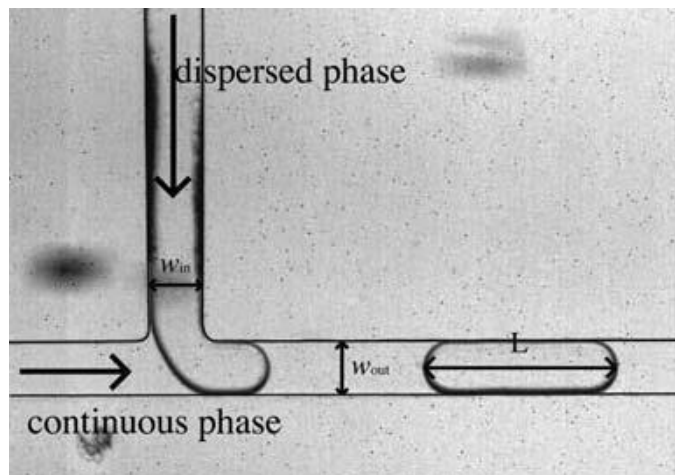
μ viscosity of the fluid (cP or kg/m.s or Pa.s)

v average flow velocity (m/s)

γ surface tension (N/m)

- Dimensionless number
- Ratio between the viscous forces and the interfacial forces

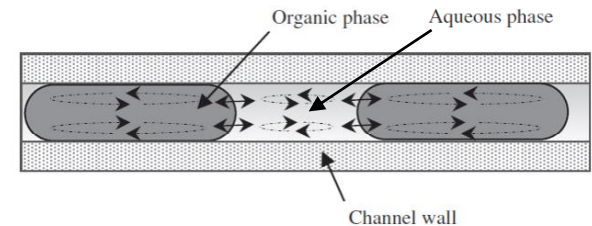
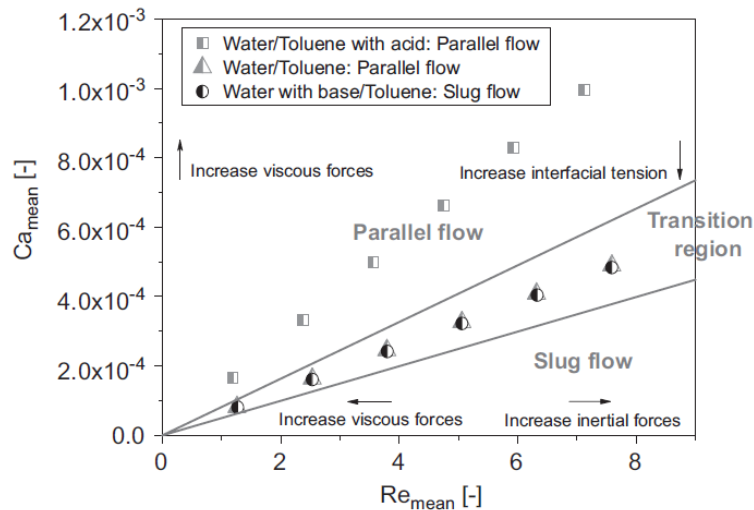
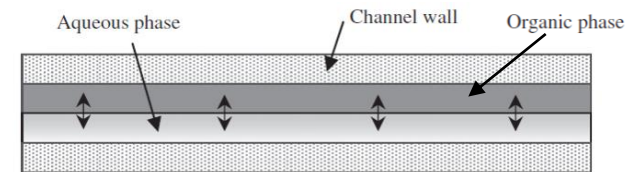
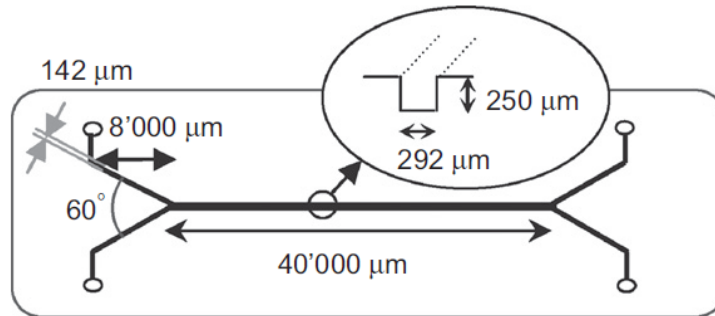
Droplet formation $\Leftrightarrow$ interfacial forces dominant, so low Ca



- Deviation in size distribution $< 1\text{-}3\%$!!!!
- Addition of surfactants in the aqueous phase for droplet stabilization

Parallel versus segmented flow

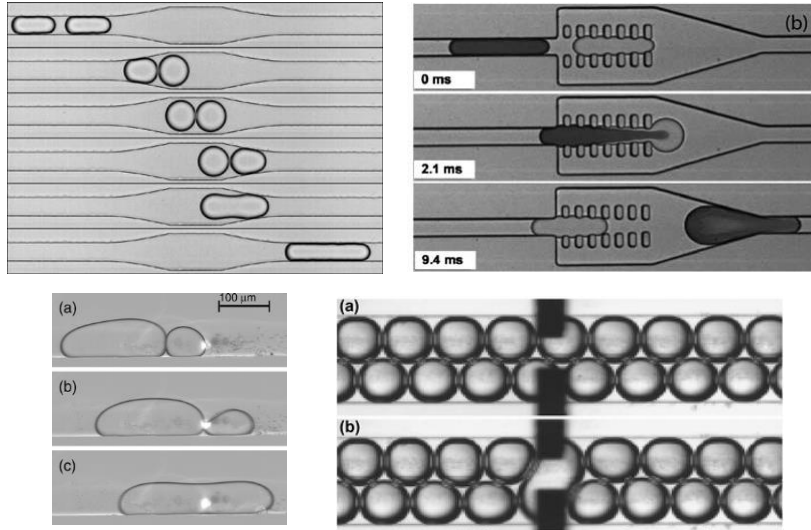
$$Ca = \frac{\mu v}{\gamma}$$



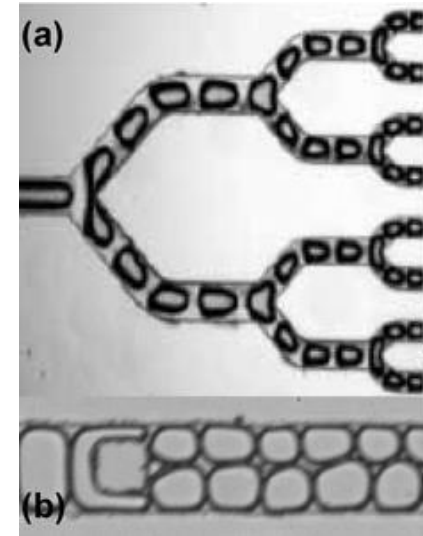
$$Re = \frac{\rho v l}{\mu}$$

Droplet microfluidic: the toolbox

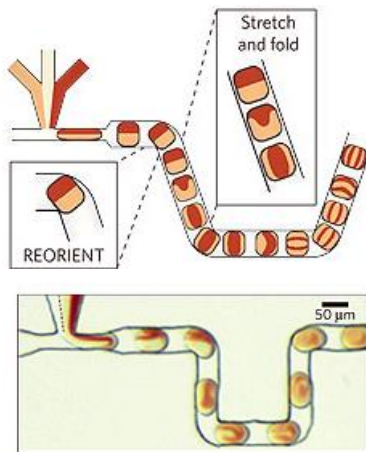
Droplet fusion



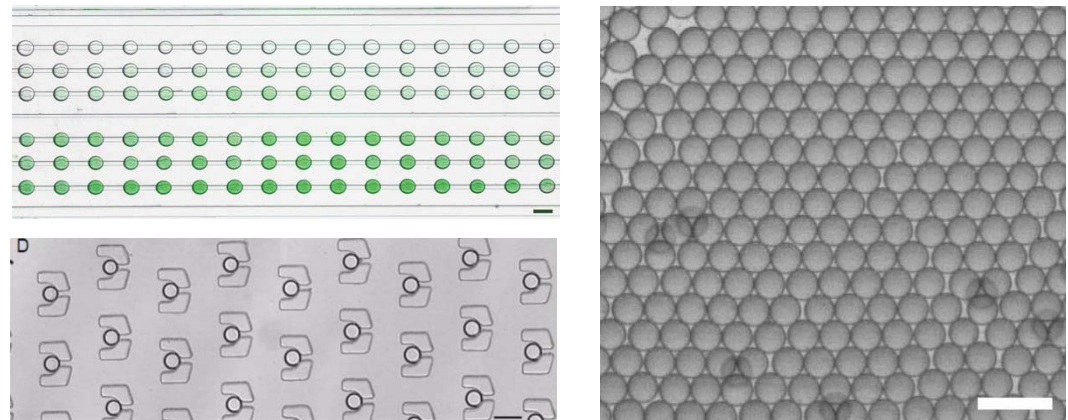
Droplet fission



Droplet mixing

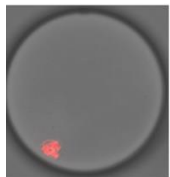
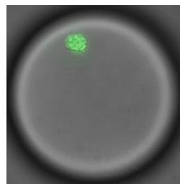
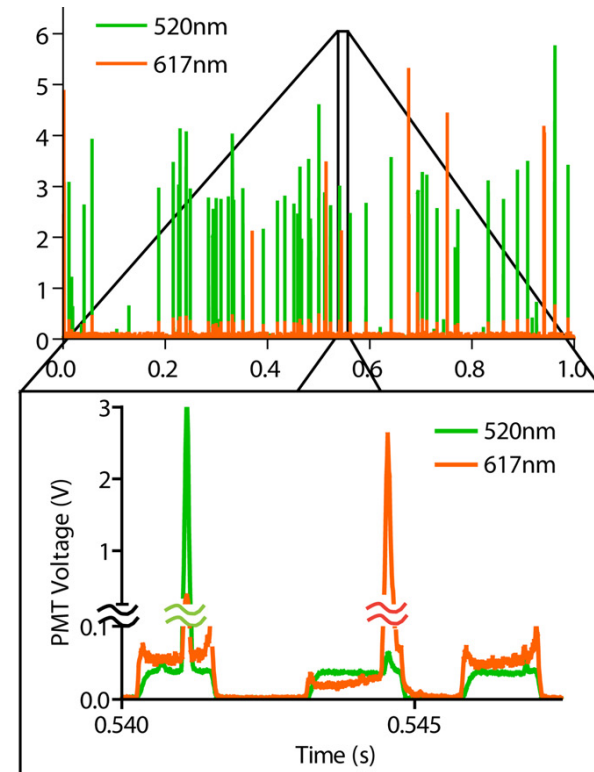
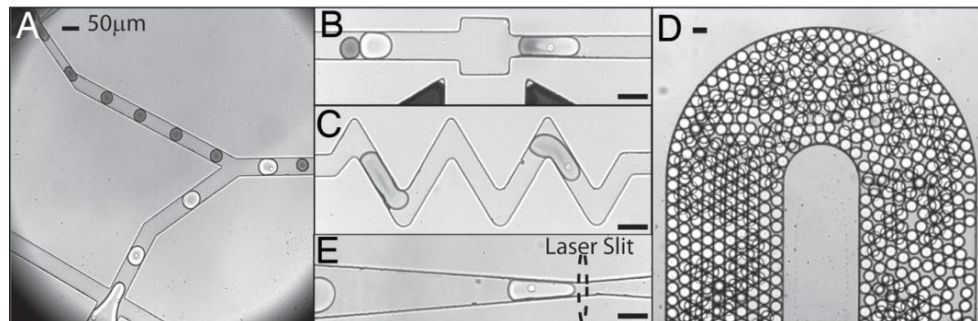
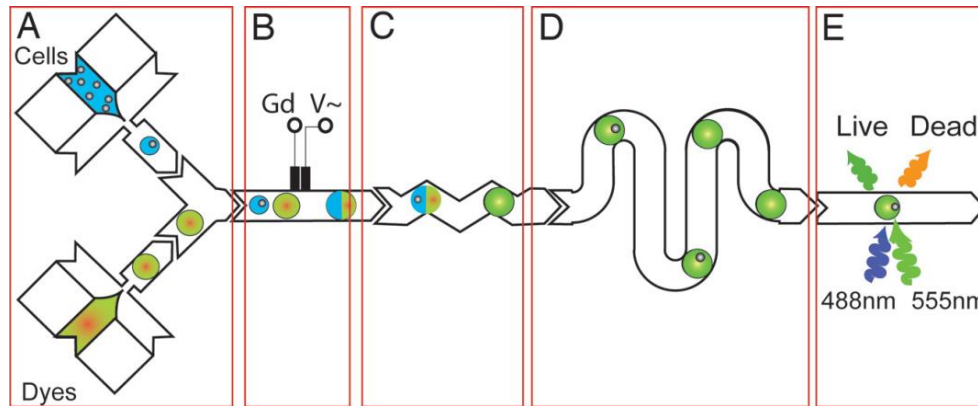


Droplet incubation - parking

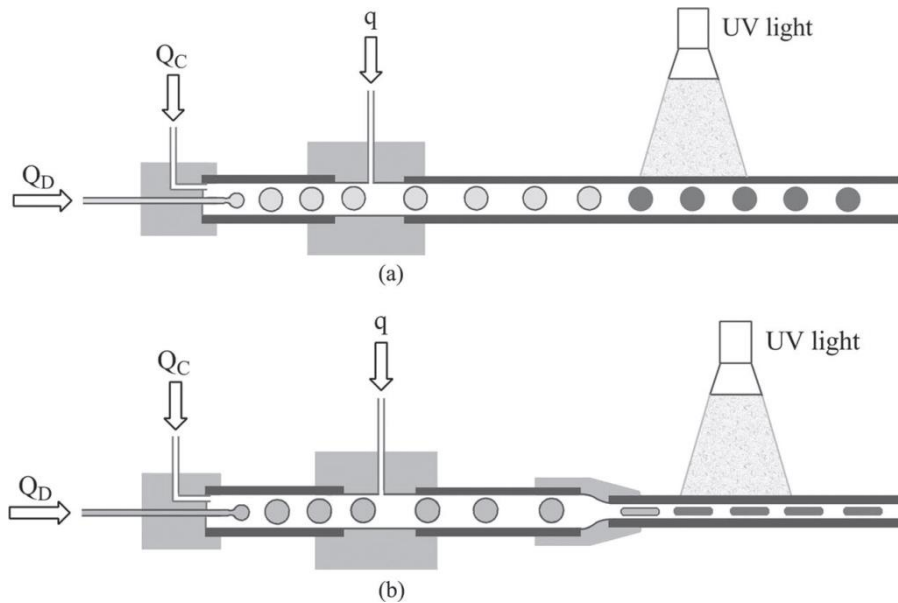


Droplet microfluidic – single cell analysis

- Encapsulation of single cells in droplets: generation of 100-1000 droplets/s
- Incubation with specific drugs and on-chip read-out (live/dead assay)
- Drug-loaded droplets encoded with a dye for drug identification
- Cell viability determined with a live/dead assay (green cells viable; red cells dead)

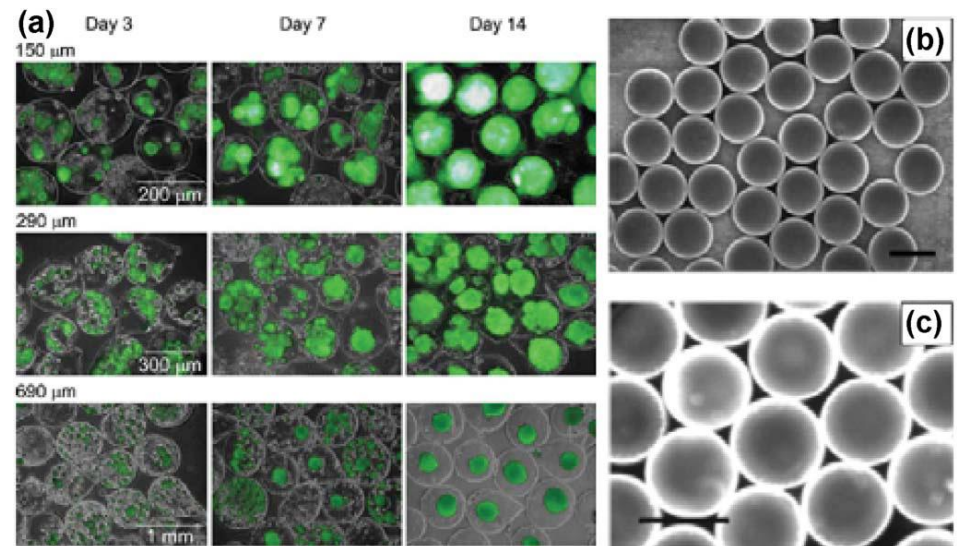


Droplet microfluidic – particle polymerization



- Addition of polymerizing agents in the aqueous (disperse) phase
- Polymerization initiated using, e.g., UV light
- Shape of the particle dictated by fluidic structure

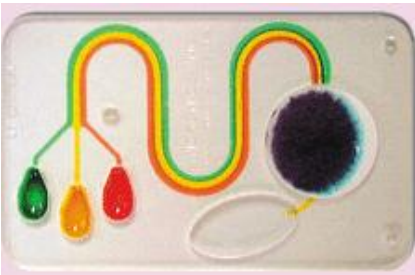
- Examples of hydrogel particles loaded with cells (green objects)
- Polymer nanoparticles
- Encapsulation of smaller beads in “larger” particles



Conclusion

- **Microfluidic devices**

- **Laminar flow** profile: deterministic behavior, highly controlled environment
- **Reynolds number**: transition between turbulent and laminar flow



$$Re = \frac{\rho v l}{\mu}$$

ρ density of the fluid (kg/m^3)

v average flow velocity (m/s)

l characteristic length of the flow (m)

μ viscosity of the fluid (cP or kg/m.s or Pa.s)

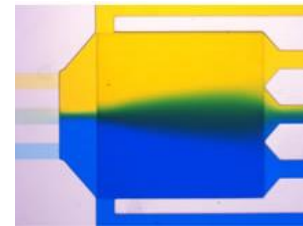
- **Diffusion**: important phenomenon at the microscale
- **Mixing** depending upon diffusion under a laminar flow configuration

$$t = \frac{L^2}{2D}$$

t diffusion time (s)

L distance traveled by diffusion (m)

D diffusion coefficient (m^2/s)



- **Pumping** liquids at the microscale: hydrodynamic, electro-osmotic, passive, centrifugal, peristaltic pumping etc..
- **Important platforms**: laminar flow (Y-shape configuration); droplet microfluidics